



The Open Petroleum Engineering Journal

Content list available at: www.benthamopen.com/TOPEJ/

DOI: 10.2174/1874834101811010067



RESEARCH ARTICLE

Modelling of Sub-Sea Gas Transmission Pipeline to Predict Insulation Failure

Ode Samson Chinedu¹, Okoro Emeka Emmanuel^{2,*}, Ekeinde Evelyn Bose¹ and Dosunmu Adewale¹¹Petroleum Engineering Department, University of Port Harcourt, Port Harcourt, Nigeria²Petroleum Engineering Department, Covenant University Ota, Ota, Nigeria

Received: August 15, 2017

Revised: April 18, 2018

Accepted: May 02, 2018

Abstract:

Background:

Thermally insulated subsea production and transmission systems are becoming more common in deep-water/ offshore operations. Premature failures of the insulation materials for these gas transmission pipelines have had significant operational impacts. The ability to timely detect these failures within these systems has been a very difficult task for the oil and gas industries. Thus, periodic survey of the subsea transmission systems is the present practice. In addition, a new technology called optic-fibre Distributed Temperature Sensing system (DTS) is now being used to monitor subsea transmission pipeline temperatures; but this technology is rather very expensive.

Objective:

However, this study proposed a model which will not only predict premature insulation failure in these transmission pipelines; but will also predict the section of the transmission line where the failure had occurred.

Methods:

From this study, we deduced that in gas pipeline flow, exit temperature for the system increases exponentially with the distance of insulation failure and approaches the normal operation if the failure occurs towards the exit of the gas pipe. This model can also be used to check the readings of an optic-fibre distributed temperature sensors.

Result and Conclusion:

After developing this model using classical visual basic and excel package, the model was validated by cross plotting the normal temperature profiles of the model and field data; and R-factor of 0.967 was obtained. Analysis of the results obtained from the model showed that insulation failure in subsea gas transmission pipeline can be predicted on a real-time basis by mere reading of the arrival temperature of a gas transmission line.

Keywords: Gas Transmission Pipeline, Insulation failure, Subsea, Temperature, Failures, Operation.

1. INTRODUCTION

Generally, when fluids flow in pipelines, there are decreases in pressure (pressure drop) as a result of friction resistances along the lines of flow. This drop in pressure also leads to temperature drop and because gas is compressible, other physical properties like density change along the pipe [1].

Thermally insulated subsea production systems are becoming more common in deepwater completions for hydrate or wax control. Premature failures of the insulation materials for these systems have had significant operational impact.

* Address correspondence to this authors at the Petroleum Engineering Department, Covenant University Ota, Ota, Nigeria; Tel: +2348066287277; E-mail: emeka.okoro@covenantuniversity.edu.ng

Syntactic foams or solid polymer insulation are currently the industry standard for subsea completion equipment. The types of insulation commonly used, their failure modes, and improved methods for selecting and qualifying these insulation systems are usually provided. For deep water application, so-called “wet” insulation systems are preferred, because the insulation can be molded directly around the equipment without the need for an outer protective jacket [2]. The insulation is exposed directly to the sea water on the outer surface, with the inner surface exposed to the high temperature operation. The critical parameters in design are the thermal conductivity, insulation thickness, and specific heat capacity [3].

However, if insulation fails then there will be additional heat losses, due to frictional resistances [4]. Thus, the gas will be delivered at a lower temperature which may condense and freeze, forming hydrates, obstructing piping and equipment, with possible adverse consequences, including explosion. In addition, insulation failure also exposes the pipeline to external corrosion hence affecting the integrity of the gas pipe [5].

In the oil and gas industry, periodic survey (mostly 5 yearly) of subsea pipelines using Remotely Operated Vehicles (ROVs) is usually carried out. In between these survey periods, insulations /coatings sometimes fail without being noticed and hence expose the pipeline to adverse corrosion and sometimes causes operational instability.

One way to reduce costs is to better optimize the maintenance strategy. Performing maintenance in subsea environments can be challenging because of harsh environmental conditions. By applying failure mechanism models it could be possible to predict equipment degradation rates and estimate the remaining equipment lifetime based on some controllable input parameters. The operation could then be optimized for maintenance, safety and cost, which would be beneficial for both the company and the environment. Thus, a single model which can predict insulation failure on a gas transmission line and the point along the pipeline where this failure will occur on a real time basis by using the gas arrival temperature as an indicator is vital. This will ensure timely intervention on the affected parts, prevent pipeline failures and reduce operational upsets. This model can also be used to validate the readings of an Advanced Fibre-Optic Distributed Temperature Sensors (DTS) in a gas transmission line equipped with DTS as is a common practice in the oil and gas industry.

2. NATURAL GAS TRANSPORTATION

The efficient and effective movement of natural gas from producing regions to consumption regions requires an extensive and elaborate transportation system. The transportation system for natural gas consists of a complex network of pipelines, designed to quickly and efficiently transport natural gas from its origin, to areas of high natural gas demand. Another method of transporting natural gas is by carriers (LNG carriers) where liquefied natural gas are stored in specially designed spherical vessels and transported by ship. This is usually a preferred means of gas transportation when pipeline transportation is not economically feasible; like in situation of very long distances, difficult terrain, and political concerns [6].

In order to ensure the efficient and safe operation of the extensive network of natural gas pipelines, pipeline companies routinely inspect their pipelines for corrosion and defects [7].

The ability of a material to retard the flow of heat is expressed by its thermal conductivity (for unit thickness) or conductance (for a specific thickness). Low values for thermal conductivity or conductance (or high thermal resistivity or resistance value) are characteristics of thermal insulation [8]. Thermal insulations are produced from many materials or combinations of materials in various forms, sizes, shapes, and thicknesses.

The insulation is added to reduce heat losses from the pipe. The addition of insulation should save money through reduced heat losses; on the other hand, the insulation material can be expensive. The trade-off between energy cost and capital cost, and the optimum insulation thickness, can be determined by optimization [9]. The optimum thickness is determined to be the point where the last dollar invested in insulation results in exactly \$1 in energy-cost savings [10]. This is considered as optimum Return on Investment by Rubin [11].

2.1. Limitation of Previous Work

Boyun Guo, Shengkai Duan, and Ali Ghalambor [12] researched on Simple Model for Predicting Heat Loss and Temperature Profiles in Insulated pipelines. The study presented three analytical heat-transfer solutions. They are the transient-flow solution for start-up mode, steady-state flow solution for normal operation mode, and transient-flow solution for flow-rate-change mode (shutting down is a special mode in which the flow rate changes to zero). An application case is illustrated in which the model-calculated temperature profiles were used for insulation design. They

did not consider cases of insulation failure in insulated gas pipelines. Hence, the models cannot predict insulation failure in real time that would engender cost effective and immediate remedial measures in gas transmission pipelines.

Other literatures showed an overview of different models developed to illustrate important failure mechanisms in subsea equipment and how they can be modelled. These models are Model by Salama [13] - which includes particle diameter as well as fluid mixture density to take into account multi-phase flows, the model by Shirazi *et al.* is a mechanical/empirical model. Mechanical calculations are used to find the impact velocity of the particle, while empirical models are used to find the erosion rate in tees and elbows based on the impact velocity. Model by McLaury and Shirazi [14] which is the Modelling of sand erosion in multi-phase flows is more complex than modelling sand erosion in single-phase flow. Mazumder *et al.* [15] developed a model based on the mechanistic model by Mclaury and Shirazi.

The most common subsea equipment has been described along with their common failure mechanisms. The most common failure mechanisms in subsea equipment were found to be sand erosion, corrosion and mechanical failure.

3. MODELING GAS PIPELINE FLOW

Generally, when fluids flow in pipelines, there are decreases in pressure (pressure drop) because of friction resistances along the lines of flow. Several empirical correlations exist in theory to predict how pressure changes/drops along the pipes during gas flow by relating pressure drop to fluid velocity, fluid physical properties and pipe geometry.

This drop in pressure also leads to temperature drop and because gas is a compressible fluid, other physical properties like density and viscosity change along the pipe. Thus, these changes are modeled and expressed as follows:

- I. One of the key assumptions here is plug flow, which means that the fluid velocity profile is plug shaped; in other words, uniform at all radial positions. Since the tube/pipe is usually too long, the temperature and pressure difference is quite significant, then the physical properties of the fluid (like density, viscosity) will change significantly.
- II. So the second step is to express this and other assumptions as a list:
- III. A steady-state solution is desired.
- IV. Perfect insulation is assumed, thus the wall temperature is constant and uniform (*i.e.*, does not change in the *z* or *r* direction) at a value T_w .
- V. The inlet temperature is constant and uniform (does not vary in *r* direction) at a value T , where $T > T_w$.
- VI. The velocity profile is plug shaped or flat, hence it is uniform with respect to *z* or *r*.
- VII. The fluid is well-mixed (highly turbulent), so the temperature is uniform in the radial direction.
- VIII. Thermal conduction of heat along the axis is small relative to convection.

The third step was the sketch that illustrates a differential volume element of the system (in this case, the flowing fluid) that was modeled. This elemental volume, which is sometimes called the “control volume” is illustrated in the Fig. (1).

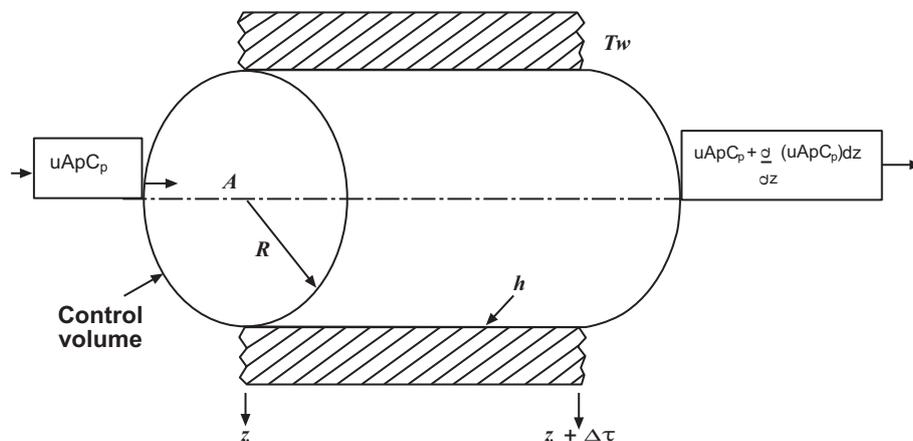


Fig. (1). Elemental or control volume for plug flow model.

We act upon this elemental volume, which spans the whole of the tube cross section, with this general conservation law:

$$\text{Rate in} - \text{Rate out} + \text{Rate of Generation} = \text{Rate of Accumulation} \quad (1)$$

Since steady state is stipulated, the accumulation of heat is zero. Moreover, there are no chemical, nuclear, or electrical sources specified within the volume element, so heat generation is absent. The only way heat can be exchanged in this system is through the perimeter of the element by way of the temperature difference between wall and fluid.

The incremental rate of heat removal were expressed as a positive quantity using Newton's law of cooling, that is,

$$AQ = (2\pi R \Delta z)h [T - T_w] \quad (2)$$

As a convention, we expressed all such rate laws as positive quantities, invoking positive or negative signs as required for the expressions in conservation law (Eq. 1). The contact area in this simple model is simply the perimeter of the element multiply by its length. The constant heat transfer coefficient is denoted by h .

Now, along the axis, heat can enter and leave the element only by convection flow, so we can write the elemental form of Eq. 1 as:

$$uA\rho C_p T - \left\{ uA\rho C_p T + \frac{\partial}{\partial z} (uA\rho C_p T) dz \right\} - (2\pi R \Delta z)h [T - T_w] = 0 \quad (3)$$

(Rate heat flow in) (Rate heat flow out) (Rate heat loss through wall)

The first two terms are simply mass flow rate multiplied by local enthalpy, where the reference temperature for enthalpy is taken as zero. If $C_p(T - T_{ref})$ was used for enthalpy, the term T_{ref} will be cancelled in the elemental balance.

Simplifying then yields the sought-after differential equation

$$uAC_p \frac{\partial}{\partial z} (\rho T) dz - (2\pi R dz)h [T - T_w] = 0 \quad (4)$$

Where the negative signs have been cancelled.

Before solving this equation, it is good practice to group parameters into a single term (lumping parameters). For such elementary problems, it is convenient to lump parameters with the lowest order term as follows:

$$\frac{\partial}{\partial z} (\rho T) dz - \frac{dz(2\pi R)h}{uAC_p} [T - T_w] = 0 \quad (4b)$$

$$\frac{\partial}{\partial z} (\rho T) - \frac{(2\pi R)h}{uAC_p} [T - T_w] = 0$$

$$\frac{\partial}{\partial z} (\rho T) - \lambda [T - T_w] = 0$$

Where, $\frac{(2\pi R)h}{uAC_p} = \lambda$

However, to solve the above equation requires a functional relationship between T and ρ for the gas, which were derived from the general gas law to be:

$$\rho = \frac{PM_w}{zPT} \quad (5)$$

Showing the inverse relationship between temperature and density for gases where:

M_w = molecular weight of the gas stream and z = the compressibility factor.

Numerous Equations of State (EOS) models have been developed. Suffice it to say that polynomial equations that are cubic in molar volume offer the best compromise of accurately describing the behavior of fluids over wide range of operating conditions. They include: Van der Waal, Redlich-Kwong (RK), Soave-Redlich-Kwong (SRK), and Peng-Robinson (PR), equation of states. SRK and PR EOS have been found to provide results sufficiently accurate for engineering purposes, they are given below:

$$P = \frac{RT}{V_i - b_i} - \frac{a_i}{V_i(V_i - b_i)} \quad (6)$$

Where the EOS parameters, a_i and b_i are given for each model as follows:

For SRK:

$$a_i = 0.42748 \frac{R^2 T_{c,i}^2}{P_{c,i}} \left\{ 1 + (0.480 + 1.574 w_{w,i} - 0.176 w_{w,i}^2) \left(1 - T_{r,i}^{1/2} \right) \right\}^2 \quad (7)$$

$$b_i = \frac{0.08664 R T_{c,i}}{P_{c,i}}$$

For PR:

$$a_i = 0.457235 \frac{R^2 T_{c,i}^2}{P_{c,i}} \left\{ 1 + (0.37464 + 1.54226 w_{w,i} - 0.26992 w_{w,i}^2) \left(1 - T_{r,i}^{1/2} \right) \right\}^2 \quad (8)$$

$$b_i = \frac{0.07769 R T_{c,i}}{P_{c,i}} \quad (9)$$

Where

$T_{c,i}$ is the critical temperature of component i

$P_{c,i}$ is the critical pressure of component i

$T_{r,i}$ is the reduced temperature of component i , $T_{r,i} = T_{c,i}/T$

w_i is the acentric factor, which is actually the vapour pressure at $0.7T_{r,i}$

Vapor viscosity is accurately correlated as a function of temperature by the relation:

$$\mu_v = \frac{AT^B}{1 + \frac{C}{T} + \frac{D}{T^2}} \quad (10)$$

Constants A, B, C, D for about 1500 compounds for both viscosities are available in the DIPPR (AIChE Design Institute for Physical Property Data).

However, for prediction of the vapor viscosity of pure hydrocarbons at low pressure (below T_{ref} of 0.6), only the molecular weight, the critical temperature, and the critical pressure are required as follows:

$$\mu_y = 4.60 \times 10^{-4} N M^{12/23} T_c^{-1/2}$$

$$N = 0.0003400 T_c^{0.04} \text{ for } T_c \leq 1.5$$

$$N = 0.0001778 (4.58 T_r - 1.67)^{0.025} \text{ for } T_r > 1.5 \quad (11)$$

The resultant viscosity is in centipoises (mPa·sec), if T_c and P_c are given in K and Pa, respectively.

Thus, because of the implicit relationships in the above equations, their evaluation involves iterative techniques *via* software.

3.1. Heat Transfer in Pipelines

The basic equation for the analysis of heat conduction is Fourier's law, which was based on experimental observations and is

$$q_n = -k_n \frac{\partial T}{\partial n} \quad (12)$$

Where the heat flux q_n (W/m^2) is the heat transfer rate in the n direction per unit area perpendicular to the direction of heat flow. k_n ($\text{W}/\text{m} \cdot \text{K}$) is the thermal conductivity in the direction n , and $\partial T / \partial n$ (K/m) is the temperature gradient in the direction n .

Thus the general equation of heat conduction in pipe (cylindrical coordinate system) was derived by performing an energy balance in conjunction with Fourier's law:

$$\frac{1}{r} \frac{\partial}{\partial r} \left(kr \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial}{\partial \phi} \left(k \frac{\partial T}{\partial \phi} \right) + \frac{\partial}{\partial z} \left(k \frac{\partial T}{\partial z} \right) + q \stackrel{\cdot}{=} \rho c \frac{\partial T}{\partial t} \quad (13)$$

3.1.1. Application

Fig. (2) showed a hollow pipe of inside radius r_1 , outside radius r_2 , length L , and thermal conductivity k . The inside and outside surfaces are maintained at constant temperatures $T_{s,1}$ and $T_{s,2}$, respectively with $T_{s,1} > T_{s,2}$ for steady-state conduction.

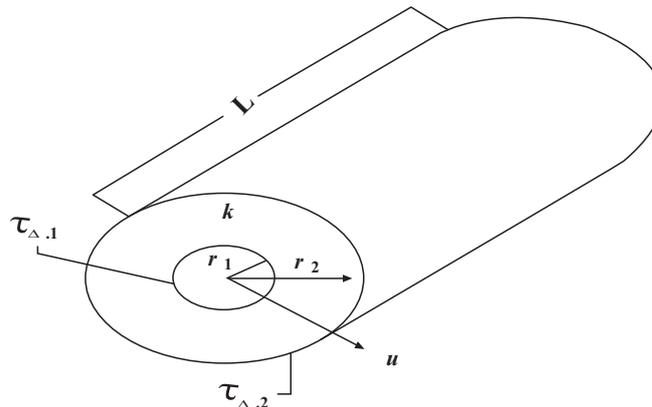


Fig. (2). Radial conduction through a hollow cylinder.

$$\frac{d}{dr} \left(r \frac{dT}{dr} \right) = 0 \quad (14)$$

In the radial direction with no internal heat generation and constant thermal conductivity, the appropriate form of the general heat conduction equation, eq. (13), is

With the boundary conditions expressed as:

$$T(r = r_1) = T_{s,1} \text{ and } T(r = r_2) = T_{s,2} \quad (15)$$

3.1.2. Thermal Resistance

Thermal resistance is defined as the ratio of the temperature difference to the associated rate of heat transfer. This is completely analogous to electrical resistance, which, according to Ohm's law, is defined as the ratio of the voltage difference to the current flow.

The rate of heat transfer q in a composite pipe is given by

$$q = \frac{T_{\infty,1} - T_{\infty,2}}{1/2\pi h_1 r_1 L + \text{Ln}(r_2/r_1)/2\pi k_1 L + \text{Ln}(r_3/r_2)/2\pi k_2 L + 1/2\pi h_2 r_3 L} \tag{16}$$

Note that without insulation, eq. 17 reduces to:

$$q = \frac{T_{\infty,1} - T_{\infty,2}}{1/2\pi h_1 r_1 L + \text{Ln}(r_2/r_1)/2\pi k_1 L + 1/2\pi h_2 r_2 L} \tag{17}$$

Also for this case, where there is coating to prevent corrosion, equations 17 and 18 become:

$$q = \frac{T_{\infty,1} - T_{\infty,2}}{1/2\pi h_1 r_1 L + \text{Ln}(r_2/r_1)/2\pi k_1 L + \text{Ln}(r_3/r_2)/2\pi k_2 L + \text{Ln}(r_4/r_3)/2\pi k_3 L + 1/2\pi h_2 r_4 L} \tag{18}$$

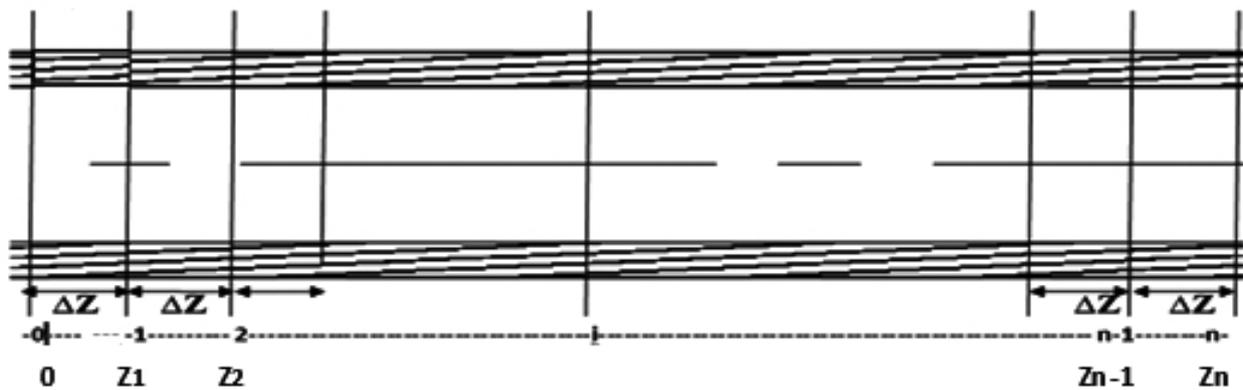
$$q = \frac{T_{\infty,1} - T_{\infty,2}}{1/2\pi h_1 r_1 L + \text{Ln}(r_2/r_1)/2\pi k_1 L + \text{Ln}(r_3/r_2)/2\pi k_2 L + 1/2\pi h_2 r_3 L} \tag{19}$$

3.2. Simulation

Thus using the above equations, one will simulate the system to predict the following:

- Temperature profile for insulated (normal operation) system
- Temperature profile for a failed insulation system

This involved numerical techniques. For these purposes the pipe is divided into grids or Sections $\Delta Z = Z_i - Z_{i-1}$ as shown in figure below:



Modelling the system, the total heat loss for the entire pipe in each case from the exit temperature were computed from the formula:

$$\text{Outlet (arrival) temp, } T_{\text{out}} = T_{\text{in}} - Q / (M.C_p) \tag{20}$$

Where M = mass flow rate of the gas = ρuA

Total heat loss for the pipeline, Q is found as the summation of heat losses in each segment, Q_i

Thus,

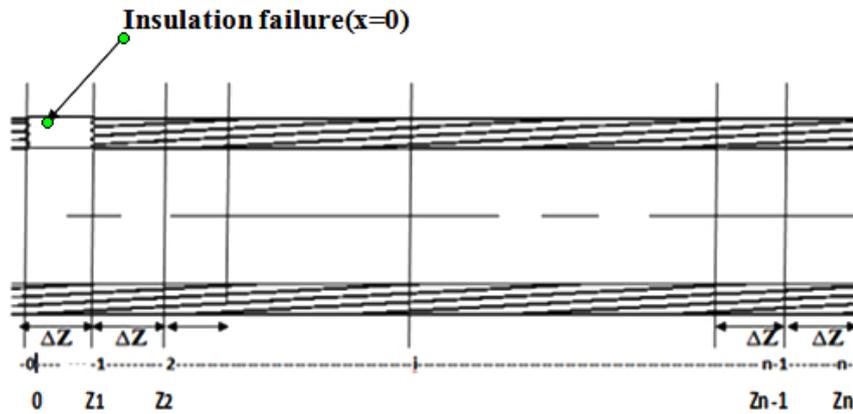
$$Q = \sum Q_i$$

For the normal operation (without insulation failure) Q_i was found by calculating for each segment as follows

$$Q_i = \frac{T_i - T_w}{1/2\pi h_1 r_1 L + \ln(r_2/r_1)/2\pi k_1 L + \ln(r_3/r_2)/2\pi k_2 L + \ln(r_4/r_3)/2\pi k_3 L + 1/2\pi h_o r_4 L} \tag{21}$$

The computed outlet temperature was compared with the operating value. Once the model predicts the operating value of the exit temperature, (at least within statistical level of significance) then a plot of T_i vs Z_i was made to give the temperature profile for normal operation. Then, the model was deployed for the more rigorous analysis for failed system as shown below:

In this category, insulation failure in each segment (grid) were considered with the assumption that insulation failure implies insulation thickness, $x = 0$. For insulation failure in the 1st segment, the diagram is as follows:



As previously shown, the total heat loss (from where the exit temperature is evaluated) is the summation of the heat losses in each segment, with the segment where insulation failure occurred evaluated. Equation 22 was adopted in this case as:

$$Q_i = \frac{T_i - T_w}{1/2\pi h_1 r_1 L + \ln(r_2/r_1)/2\pi k_1 L + \ln(r_3/r_2)/2\pi k_2 L + 1/2\pi h_o r_3 L} \tag{22}$$

While all the other segments without insulation failure were evaluated using equation 21.

4. RESULTS AND DISCUSSION

The study model was validated using the field data in Table 1 and the length of the pipe under consideration is 55 kilometers.

Table 1. Field data for 55Km Subsea Pipeline and Coating Data

Pipeline Designation		24" Gas Export Line	
Steel: API 5L N65			
ZONE 1	Outside diameter	mm	609.6
	Wall thickness	mm	15.9
ZONE 2	Outside diameter	mm	622.2
	Wall thickness	mm	22.2
Corrosion Allowance		mm	1.5
SMYS		Mpa	448

(Table 1) contd.....

Pipeline Designation		24" Gas Export Line
Density	Kg/M ³	7850
Young's modulus	Mpa	207.000
Poisson's ratio	-	0.3
Thermal expansion coeff.	1°C	11.7 X 10 ⁻⁶
Steel Conductivity	W/m°C	45.35
Flow Rate	Sm ³ /h	845000
Average Joint Length	m	12.2
Concrete coating: High Density Concrete		
Coating thickness	mm	50 (1)
Coating density	Kg/m ³	3040
Anti-corrosion coating: 3 Layer-Polyethylene		
Coating thickness	Mm	3.2
Coating density	Kg/m ³	965

(1) Concrete THK = 50mm at least until the content temperature equals the ambient temperature

Using the data in conjunction with the above model equations 1 to 10, temperature profiles has been calculated using a software, while the heat losses and the corresponding exit gas temperatures, for normal and insulation failure at different pipe length were calculated using equations 11 to 23.

Model Validation

The model was validated using field data as shown in Fig. (3). Actual field temperature and that calculated using the model was presented in a plotted and compared. The close match shows that the model can predict the temperature distribution of an insulated gas pipeline.

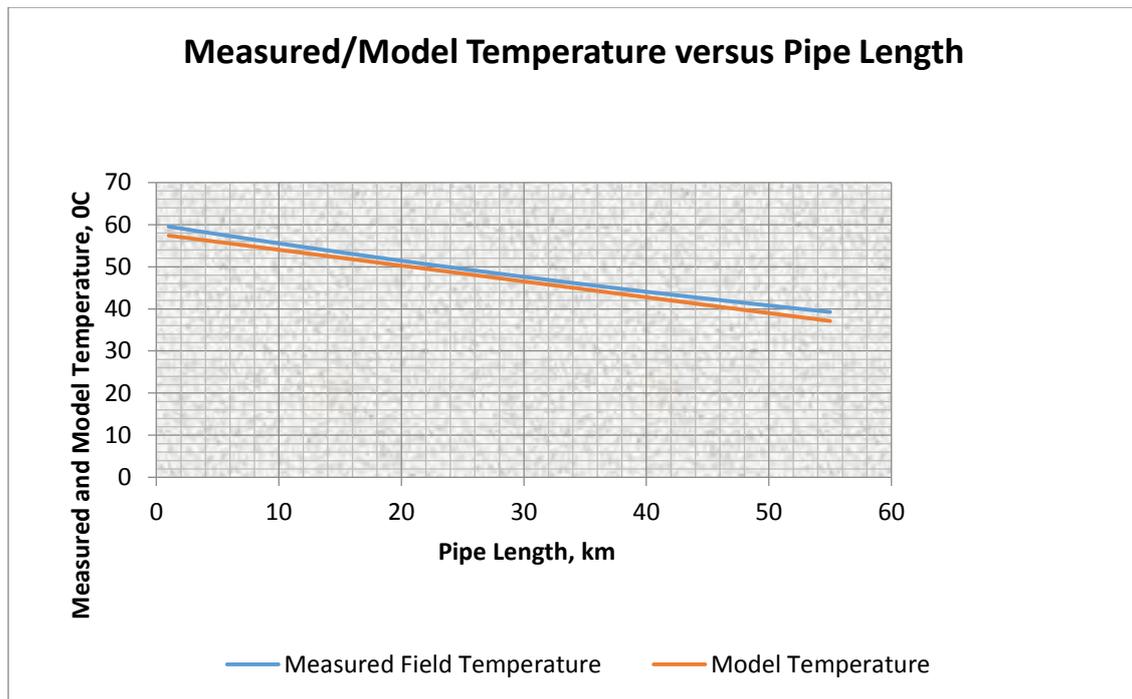


Fig. (3). A plot of Measured and Model temperature and Pipe Length.

From the Fig. (4), it is observed that the model can predict the temperature distribution in normal operation of a gas pipeline. The cross plot shows an R-Factor of 0.997 confirming the accuracy of the model.

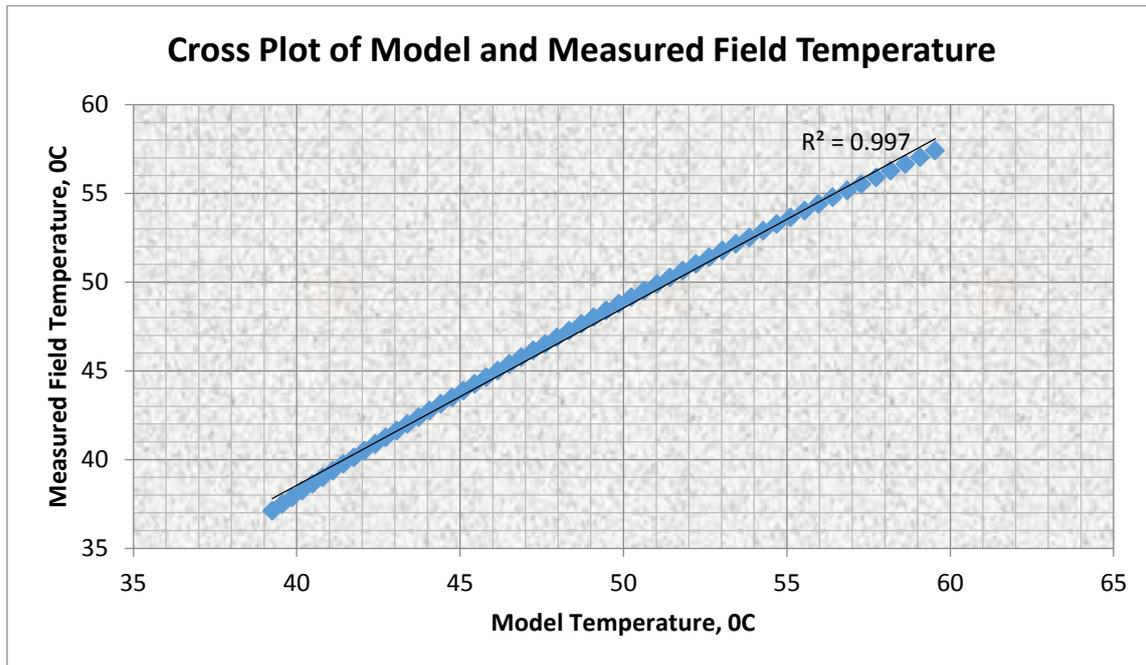


Fig. (4). A cross plot of Field Temperature Data and Model Temperatures Data.

5. DISCUSSION

Considering a pipeline system of 55 km, Table 2 gives the temperature and pressure distribution along the whole length of the pipe while Fig. (5) is the corresponding plot showing the temperature and pressure profiles along the pipe line. It can be observed that temperature and pressure decrease along the pipe line owing to frictional resistances to the flow.

Table 2. Temperature and Pressure distribution

S/N	Pipe length, km	Pressure, barg	Temp. °C	S/N	Pipe length, km	Pressure, barg	Temp. °C
1	1	1.47E+02	59.5388	29	29	1.26E+02	47.9698
2	2	1.46E+02	59.0811	30	30	1.26E+02	47.6011
3	3	1.45E+02	58.6270	31	31	1.25E+02	47.2352
4	4	1.44E+02	58.1764	32	32	1.24E+02	46.8721
5	5	1.44E+02	57.7292	33	33	1.24E+02	46.5118
6	6	1.43E+02	57.2855	34	34	1.23E+02	46.1543
7	7	1.42E+02	56.8451	35	35	1.22E+02	45.7995
8	8	1.41E+02	56.4082	36	36	1.22E+02	45.4475
9	9	1.41E+02	55.9746	37	37	1.21E+02	45.0981
10	10	1.40E+02	55.5443	38	38	1.20E+02	44.7515
11	11	1.39E+02	55.1174	39	39	1.20E+02	44.4075
12	12	1.38E+02	54.6937	40	40	1.19E+02	44.0662
13	13	1.38E+02	54.2733	41	41	1.19E+02	43.7274
14	14	1.37E+02	53.8561	42	42	1.18E+02	43.3913
15	15	1.36E+02	53.4422	43	43	1.17E+02	43.0578
16	16	1.35E+02	53.0314	44	44	1.17E+02	42.7268
17	17	1.35E+02	52.6237	45	45	1.16E+02	42.3984
18	18	1.34E+02	52.2192	46	46	1.15E+02	42.0725
19	19	1.33E+02	51.8179	47	47	1.15E+02	41.7491
20	20	1.33E+02	51.4195	48	48	1.14E+02	41.4282
21	21	1.32E+02	51.0243	49	49	1.14E+02	41.1097
22	22	1.31E+02	50.6321	50	50	1.13E+02	40.7937
23	23	1.30E+02	50.2429	51	51	1.12E+02	40.4802

(Table 2) contd.....

S/N	Pipe length, km	Pressure, barg	Temp. °C	S/N	Pipe length, km	Pressure, barg	Temp. °C
24	24	1.30E+02	49.8567	52	52	1.12E+02	40.1690
25	25	1.29E+02	49.4735	53	53	1.11E+02	39.8603
26	26	1.28E+02	49.0932	54	54	1.11E+02	39.5539
27	27	1.28E+02	48.7158	55	55	110.1411	39.2498
28	28	1.27E+02	48.3414				

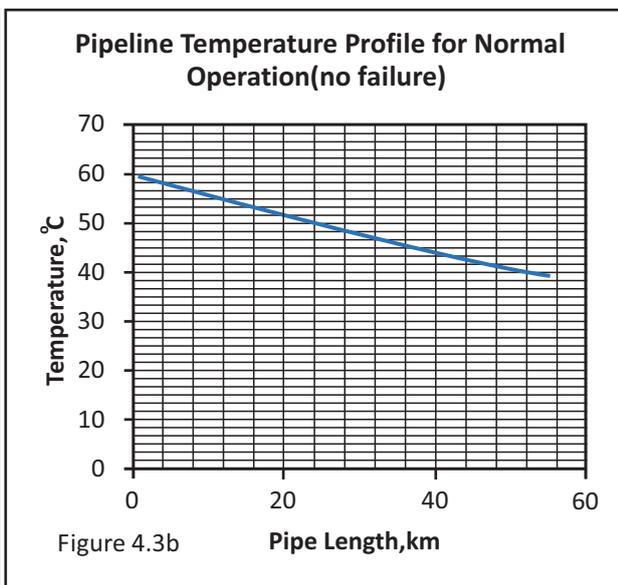
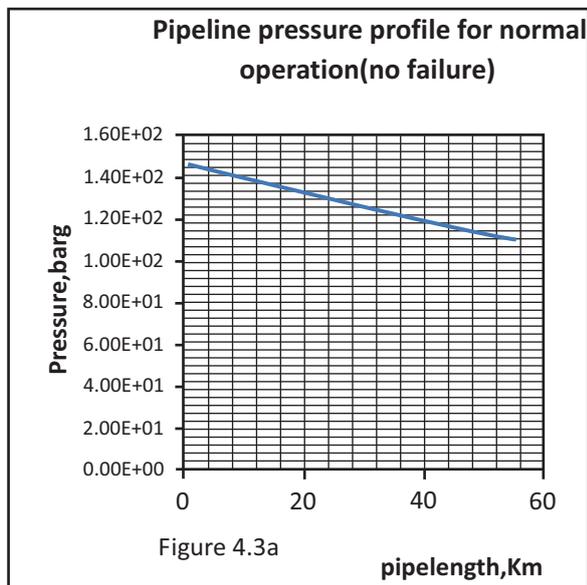


Fig. (5). A plot of Temperature versus Pipe Length.

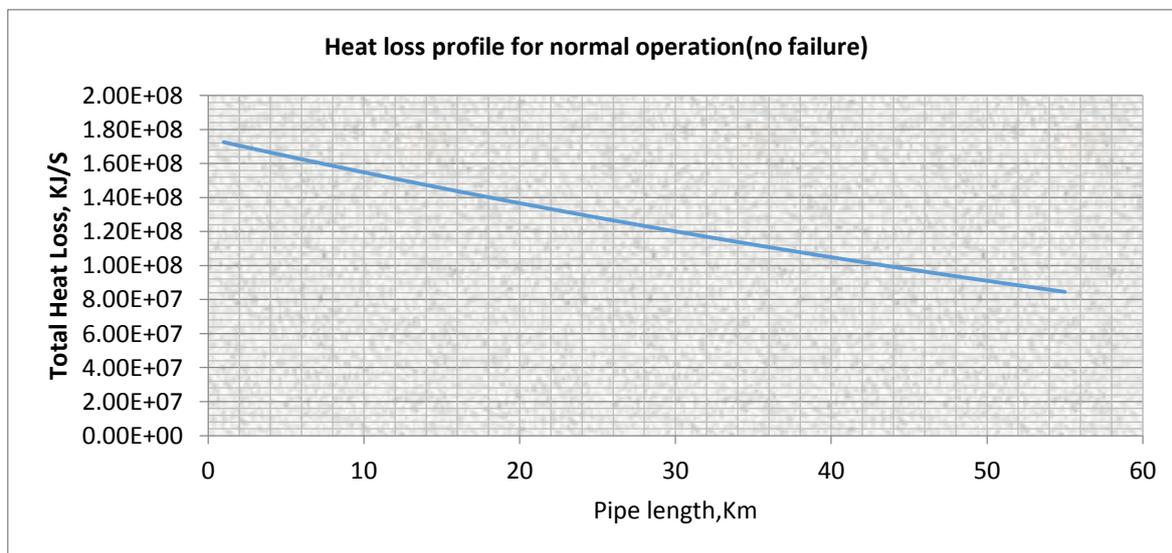


Fig. (6). A Plot of Total Heat Loss versus Pipe Length.

Table 3 gives the total energy loss for a normal operation (without insulation failure) while Fig. (6) is the corresponding total heat loss profile.

Table 3. Total Energy Loss for an Ideal Operation

S/N	Pipe length, km	Heat loss, KJ/s	S/N	Pipe length, km	Heat loss, KJ/s
1	1	1.73E+08	29	29	1.22E+08
2	2	1.71E+08	30	30	1.22E+08
3	3	1.68E+08	31	31	118511341.7
4	4	1.66E+08	32	32	116946261.9
5	5	1.64E+08	33	33	115395061.2
6	6	1.63E+08	34	34	113857584.6
7	7	1.61E+08	35	35	112333735.0
8	8	1.59E+08	36	36	110823366.9
9	9	1.57E+08	37	37	109326383.3
10	10	1.55E+08	38	38	107842667.9
11	11	1.53E+08	39	39	106372055.8
12	12	1.51E+08	40	40	104914508.1
13	13	1.49E+08	41	41	103469840.7
14	14	1.47E+08	42	42	102037975.9
15	15	1.46E+08	43	43	100618797.2
16	16	1.44E+08	44	44	99212207.9
17	17	1.42E+08	45	45	97818042.8
18	18	1.40E+08	46	46	96436234.2
19	19	1.38E+08	47	47	95066656.0
20	20	1.37E+08	48	48	93709230.6
21	21	1.35E+08	49	49	92363812.4
22	22	1.33E+08	50	50	91030304.6
23	23	1.32E+08	51	51	89708600.3
24	24	1.30E+08	52	52	88398631.8
25	25	1.28E+08	53	53	87100234.2
26	26	1.27E+08	54	54	85813339.4
27	27	1.25E+08	55	55	84537850.7
28	28	1.23E+08			

This is because the Total heat loss is a direct function of the difference between the inlet temperature and the pipe wall temperature. The higher the difference, the more heat loss along the pipe.

Table 4 gives the total energy loss for a failed insulation while Fig. (7) is the corresponding total energy loss with pipe length.

Table 4. Total Energy Loss for a Failed Insulation

S/N	Pipe length, km	Heat loss Profile, KJ/s	S/N	Pipe length, km	Heat loss Profile, KJ/s
1	1	194127513.4	29	29	136888424.3
2	2	191828353.5	30	30	135096194.2
3	3	189549553.3	31	31	133319828.6
4	4	187290916.4	32	32	131559185.5
5	5	231734394.3	33	33	129814155.8
6	6	182833543.2	34	34	128084565.0
7	7	180634392.3	35	35	126370304.0
8	8	178454739.1	36	36	124671209.1
9	9	176294387.3	37	37	122987171.3
10	10	174153162.2	38	38	121318059.4
11	11	172030900.2	39	39	119663688.2
12	12	169927415.8	40	40	118024013.9
13	13	167842589.0	41	41	116398829.2
14	14	165776212.5	42	42	114788046.9
15	15	163728144.4	43	43	113191536.0
16	16	161698210.2	44	44	111609187.3

(Table 4) contd....

S/N	Pipe length, km	Heat loss Profile, KJ/s	S/N	Pipe length, km	Heat loss Profile, KJ/s
17	17	159686257.1	45	45	110040815.6
18	18	157692121.4	46	46	108486344.2
19	19	155715617.7	47	47	106945631.5
20	20	153756658.7	48	48	105418590.1
21	21	151815026.1	49	49	103905056.3
22	22	149890600.0	50	50	102404921.1
23	23	147983216.6	51	51	100918064.4
24	24	146092712.4	52	52	99444409.9
25	25	144218967.2	53	53	97983772.0
26	26	142361795.7	54	54	96536074.4
27	27	140521088.6	55	55	95101208.0
28	28	138696682.4			

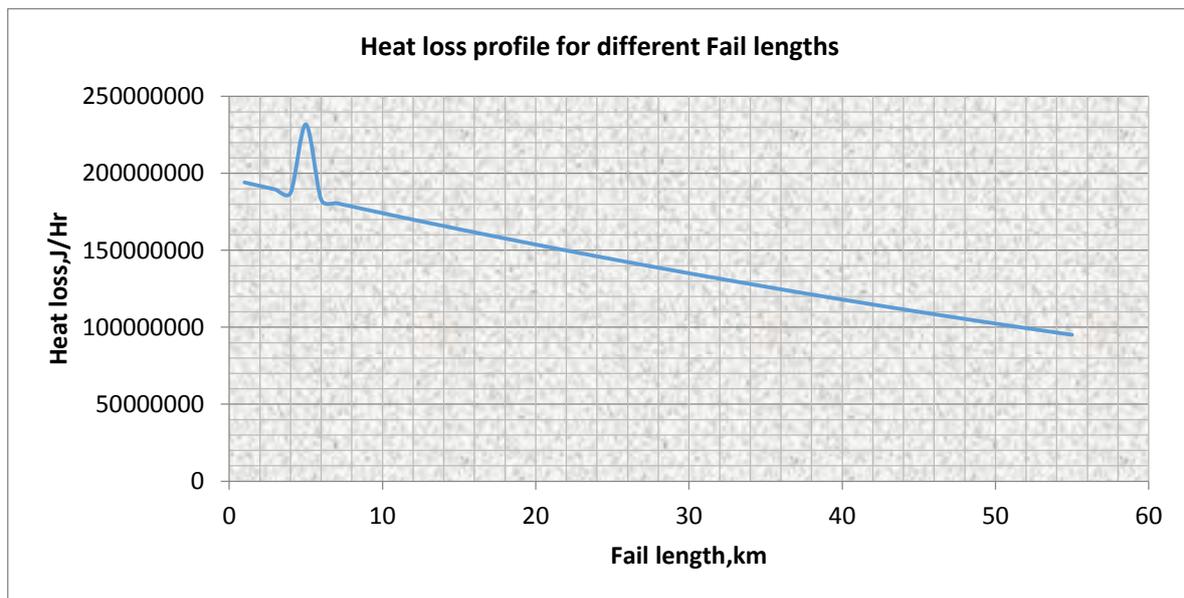


Fig. (7). Heat loss versus distance of insulation failure (insulation failed between 4 -6km)

This shows that the heat loss will increase when the insulation fails Table 5. This is as a result of inverse relationship between total heat loss and thermal resistance Fig. (8) (Insulation failure implies reduction in thermal resistance).

Table 5. Overall Heat Loss and the arrival Temperature with insulation failure length.

S/N	Fail_length, km	Total heat loss Profile, J/H	Arrival Temp. °C	S/N	Fail_length, km	Total heat loss Profile, J/H	Arrival Temp. °C
1	1	12046752652	1.91E+01	29	29	7441856882	3.47E+01
2	2	9732440872	2.70E+01	30	30	7436258695	3.47E+01
3	3	8915763463	2.97E+01	31	31	7430887366	34.77
4	4	8496160717	3.12E+01	32	32	7425712666	34.79
5	5	8241728092	3.20E+01	33	33	7420708596	34.80
6	6	8072048312	3.26E+01	34	34	7415852100	34.82
7	7	7951604227	3.30E+01	35	35	7411124410	34.84
8	8	7862223290	3.33E+01	36	36	7406508070	34.85
9	9	7793632297	3.35E+01	37	37	7401989084	34.87
10	10	7739583240	3.37E+01	38	38	7397554082	34.88
11	11	7696063954	3.39E+01	39	39	7393192574	34.90
12	12	7660379912	3.40E+01	40	40	7388893580	34.91

(Table 5) contd....

S/N	Fail_length, km	Total heat loss Profile, J/H	Arrival Temp. °C	S/N	Fail_length, km	Total heat loss Profile, J/H	Arrival Temp. °C
13	13	7630659267	3.41E+01	41	41	7384649843	34.92
14	14	7605564111	3.42E+01	42	42	7380453273	34.94
15	15	7584111477	3.42E+01	43	43	7376297318	34.95
16	16	7565567410	3.43E+01	44	44	7372176223	34.97
17	17	7549371707	3.44E+01	45	45	7368085551	34.98
18	18	7535091514	3.44E+01	46	46	7364019598	35.00
19	19	7522388073	3.45E+01	47	47	7359975697	35.01
20	20	7510992071	3.45E+01	48	48	7355949145	35.02
21	21	7500686261	3.45E+01	49	49	7351938157	35.04
22	22	7491297070	3.46E+01	50	50	7347938186	35.05
23	23	7482681102	3.46E+01	51	51	7343948753	35.06
24	24	7474720903	3.46E+01	52	52	7339967166	35.08
25	25	7467319165	3.46E+01	53	53	7335991611	35.09
26	26	7460394762	3.47E+01	54	54	7332019872	35.10
27	27	74538796673	3.47E+01	55	55	7328050556	35.12
28	28	7447716564	3.47E+01				

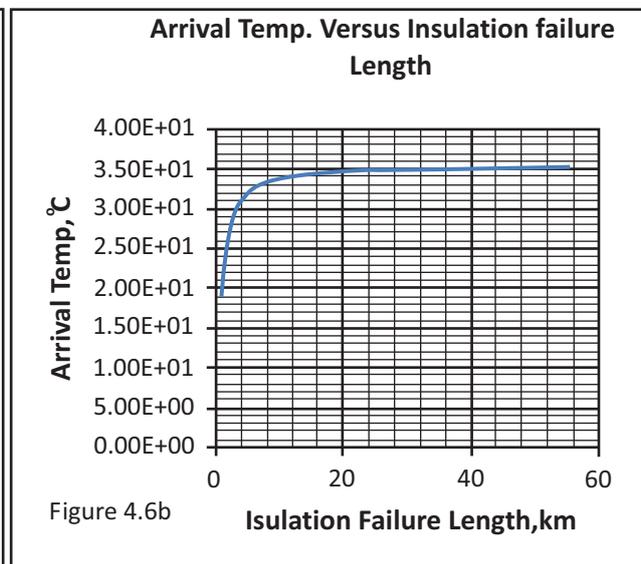
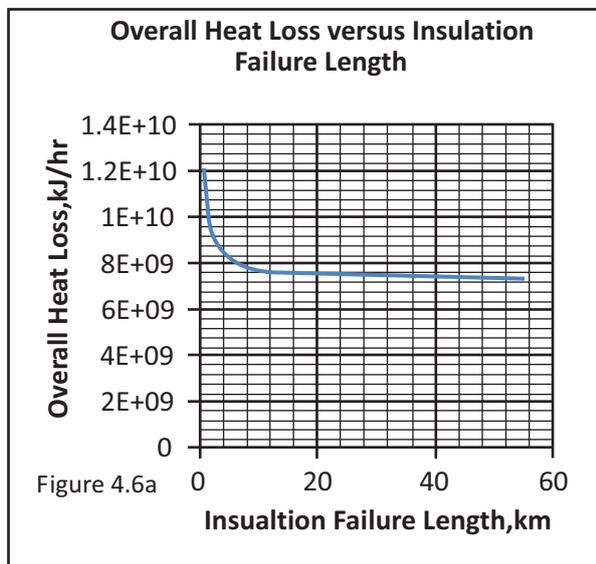


Fig. (8). A plot of Overall Heat Loss versus Insulation failure Length.

Table 6. Arrival Temperatures of Normal and Insulation Failed Operations with Pipe Length.

S/N	Fail_length, km	Arrival temp. (normal ops)	Arrival Temp. °C	S/N	Fail_length, km	Arrival temp. (normal ops)	Arrival Temp. °C
1	1	35.184	1.91E+01	29	29	35.184	3.47E+01
2	2	35.184	2.70E+01	30	30	35.184	3.47E+01
3	3	35.184	2.97E+01	31	31	35.184	34.77
4	4	35.184	3.12E+01	32	32	35.184	34.79
5	5	35.184	3.20E+01	33	33	35.184	34.80
6	6	35.184	3.26E+01	34	34	35.184	34.82
7	7	35.184	3.30E+01	35	35	35.184	34.84
8	8	35.184	3.33E+01	36	36	35.184	34.85
9	9	35.184	3.35E+01	37	37	35.184	34.87
10	10	35.184	3.37E+01	38	38	35.184	34.88
11	11	35.184	3.39E+01	39	39	35.184	34.90
12	12	35.184	3.40E+01	40	40	35.184	34.91
13	13	35.184	3.41E+01	41	41	35.184	34.92

(Table 6) contd....

S/N	Fail_length, km	Arrival temp. (normal ops)	Arrival Temp. °C	S/N	Fail_length, km	Arrival temp. (normal ops)	Arrival Temp. °C
14	14	35.184	3.42E+01	42	42	35.184	34.94
15	15	35.184	3.42E+01	43	43	35.184	34.95
16	16	35.184	3.43E+01	44	44	35.184	34.97
17	17	35.184	3.44E+01	45	45	35.184	34.98
18	18	35.184	3.44E+01	46	46	35.184	35.00
19	19	35.184	3.45E+01	47	47	35.184	35.01
20	20	35.184	3.45E+01	48	48	35.184	35.02
21	21	35.184	3.45E+01	49	49	35.184	35.04
22	22	35.184	3.46E+01	50	50	35.184	35.05
23	23	35.184	3.46E+01	51	51	35.184	35.06
24	24	35.184	3.46E+01	52	52	35.184	35.08
25	25	35.184	3.46E+01	53	53	35.184	35.09
26	26	35.184	3.47E+01	54	54	35.184	35.10
27	27	35.184	3.47E+01	55	55	35.184	35.12
28	28	35.184	3.47E+01				

It can be deduced from Fig. (9), that the arrival temperature is constant for normal operation (that is when there is no insulation failure) because the overall heat loss is constant but the arrival temperatures varies (reduces) for failed operations due to increase in the overall heat loss resulting from the reduction in thermal resistance at the pipe section where the insulation failed. The reduction in arrival temperature is pronounce when the insulation failure is closer to departure point due to high heat loss at that point and approaches the value of that of normal operation when the failure is close to the arrival point due to low heat loss at that point.

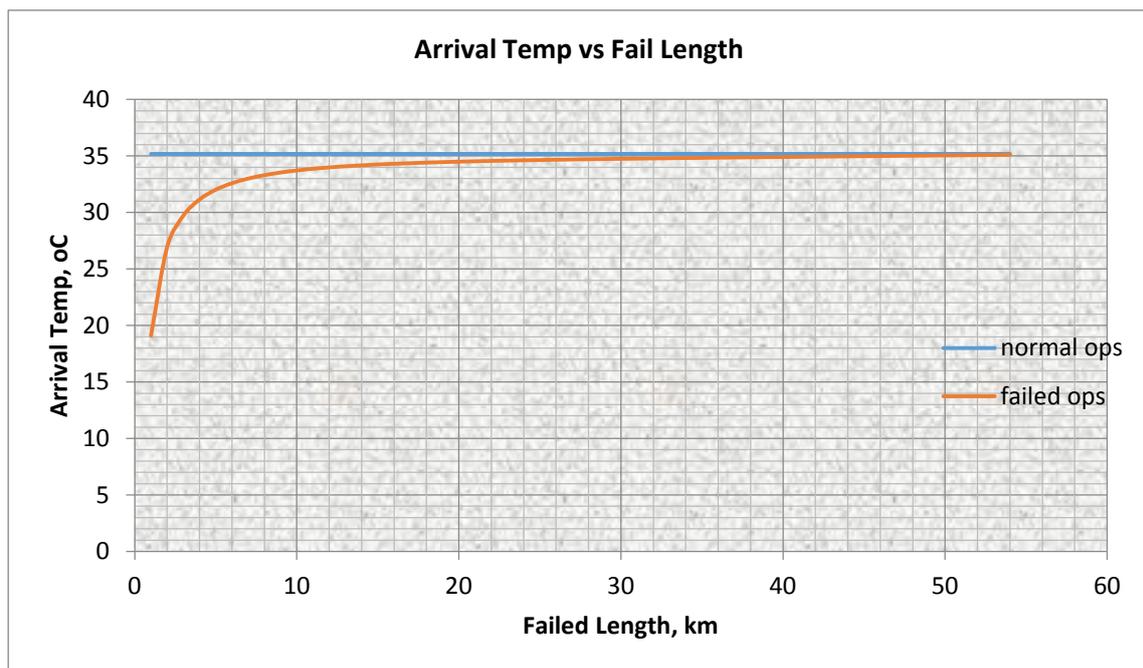


Fig. (9). A plot of Arrival Temperature versus pipe length for Normal and Insulation Failed length.

CONCLUSION

In this study, it has been shown that in gas pipeline flow, exit temperature increases exponentially with the distance of insulation failure, and approaches the normal operation if the failure occurs towards the exit of the pipe.

A predictive model that predicts insulation failure and the pipeline location where it occurred was also developed. Thus, by merely reading the exit temperature, one will not only ascertain if insulation failure has occurred, but will also know the location of the pipe where it has occurred, so that remedial measures will be promptly taken without waste of time and resources searching for the location.

In this study, we have observed the following points in the subsea gas pipeline flow:

1. The exit temperature increases exponentially with the distance of insulation failure, and approaches the normal operation if the failure occurs towards the exit of the pipe.
2. A predictive model that predicts insulation failure and the pipeline location where it occurred was proposed and developed.
3. Like all numerical techniques, the smaller the grid size, the better the results, but with increased rigour.
4. The model developed can be used to check the readings of an optic-fibre distributed temperature sensors.
5. After developing this model using classical visual basic and excel package, the model was validated by cross plotting the normal temperature profiles of the model and field data; and R-factor of 0.997 was obtained.
6. Analysis of the results from the model showed that insulation failure can be predicted on a real time basis.

CONSENT FOR PUBLICATION

Declared none.

CONFLICT OF INTEREST

The authors declare no conflict of interest, financial or otherwise.

ACKNOWLEDGEMENTS

Declared none

REFERENCES

- [1] M. Roche, D. Melot, and G. Paugam, "Recent experience with pipeline coating failures", In: *16th International Conference on Pipeline Protection, BHR Group, 2-4 November*, Paphos, Cyprus, 2005.
- [2] C. Melve, A. Rydin, and B. Hansen, "Long term testing of high temperature thermal insulation for subsea flow lines at simulated seabed conditions", *15th International Conference on Pipeline Protection*, 2010
- [3] M. Batallas, and P. Singh, "Evaluation of Anticorrosion Coatings for High Temperature Service", *NACE Corrosion, paper no. 08039*, .
- [4] B. Hansen, and C. Rydin, Development and Qualification of Novel Thermal Insulation Systems for Deepwater Flowlines and Risers based on Polypropylene. *OTC 2002, paper no. 14121 Houston.*, OTC: TX, 2002. [<http://dx.doi.org/10.4043/14121-MS>]
- [5] J.A. Beavers, Thompson NG. External corrosion of oil and natural gas pipelines. *ASM handbook*. 2006;13:1015-25.
- [6] D.R. Dott, *Optimal Network Design for Natural Gas Pipelines.*, University of Calgary: Alberta, 1997, pp. 57-90.<http://dspace.ucalgary.ca/bitstream/1880/26992/1/31387Dott.pdf>
- [7] B. Douglas, D. Pugh, C. Monahan, and P. Russ, "Top of Line Corrosion Management through Innovative Subsea Facility Design", *International Petroleum Technology Conference*, 2008 [<http://dx.doi.org/10.2523/IPTC-12788-MS>]
- [8] Turner and Malloy, *Handbook of Thermal Insulation Design Economics for Pipes and Equipment.*, Krieger: New York, 1980.
- [9] M. Aggour, *Petroleum Economics and Engineering*, edited by Abdel- Aal, H. K., Bakr, B. A., and Al-Sahlawi, M., Marcel Dekker, Inc., 1992, p. 309.
- [10] ETI- Economic Thickness for Industrial Insulation, Conservation Pap. 46, Federal Energy Administration, August 1976 Piping Insulation- Economics and Profits vol.69, 1982, pp. 27-46.
- [11] R.H. Paul, "Common law and statute law", *J. Legal Stud.*, vol. 11, no. 2, pp. 205-223, 1982. [<http://dx.doi.org/10.1086/467698>]
- [12] B. Guo, S. Duan, and A. Ghalambor, "A simple model for predicting Heat loss and Temperature profiles in Insulated pipelines", *SPE Prod. Oper.*, vol. 21, no. 1, pp. 107-113, 2006. [<http://dx.doi.org/10.2118/86983-PA>]
- [13] M.M. Salama, "An alternative to api 14e erosional velocity limits for sand-laden fluids", *J. Energy Resour. Technol.*, vol. 122, no. 2, p. 71, 2000. [<http://dx.doi.org/10.1115/1.483167>]
- [14] B.S. McLaury, and S.A. Shirazi, "An alternative method to api rp 14e for predicting solids erosion in multiphase flow", *J. of Energy Resources Techno., Transac. of the ASME*, vol. 122, no. 3, pp. 115-122, 2000. [<http://dx.doi.org/10.1115/1.1288209>]

- [15] Q.H. Mazumder, S.A. Shirazi, B.S. McLaury, J.R. Shadley, and E.F. Rybicki, A mechanistic model to predict erosion in multiphase flow in elbows downstream of vertical pipes, 2004.

© 2018 Chinedu *et al.*

This is an open access article distributed under the terms of the Creative Commons Attribution 4.0 International Public License (CC-BY 4.0), a copy of which is available at: <https://creativecommons.org/licenses/by/4.0/legalcode>. This license permits unrestricted use, distribution, and reproduction in any medium, provided the original author and source are credited.