



Contents lists available at ScienceDirect

Egyptian Journal of Petroleumjournal homepage: www.sciencedirect.com

Full Length Article

Optimization of natural gas treatment for the removal of CO₂ and H₂S in a novel alkaline-DEA hybrid scrubber [☆]Samuel Eshorame Sanni ^{a,*}, Oluranti Agboola ^a, Omololu Fagbiele ^a, Esther Ojima Yusuf ^a, Moses Eterigho Emeterie ^b^aDepartment of Chemical Engineering, Covenant University, PMB 10221, Ota, Ogun State, Nigeria^bDepartment of Physics, Covenant University, PMB 10221, Ota, Ogun State, Nigeria

ARTICLE INFO

Article history:
Received 21 February 2019
Revised 6 November 2019
Accepted 21 November 2019
Available online xxxx

Keywords:
Absorption
Acid gas
Gas treatment
Process optimization
Process simulation

ABSTRACT

Contaminated natural gas when carelessly handled, often poses human and equipment related problems ranging from lung and skin infections to corrosion, equipment fouling/failure and reduction in gas quality owing to the presence of acid gases. In this work, four natural gas (NG) samples were treated to remove CO₂ and H₂S using 10–50% Di-Ethanolamine (DEA) solutions mixed with 5% w/w 0.1 M calcium hydroxide. The treatment process gave increased acid gas removal as increased DEA concentration. Based on the simulation results, cost effective treatment of the gas sample, require 0.1 M Ca(OH)₂ and DEA mixed solutions in the range of 27.4–30%. The optimum mixture concentration for the gas treatment was found to be 30% Ca(OH)₂-DEA hybrid solution with feed gas flow rate of 8.00 kmol/h. In terms of pressure energy consumption, pumping the hybrid mix at 8.00 kmol/h will save pressure energy as compared to pumping the feed gas at 1024.58 kmol/h since the lower and upper limit feed gas flow rates gave similar results. The optimum pressure for NG treatment was found to be in the range of 2–2.7 bar (2–2.7^{10³} kgm⁻² s⁻²). © 2019 Egyptian Petroleum Research Institute. Production and hosting by Elsevier B.V. This is an open access article under the CC BY-NC-ND license (<http://creativecommons.org/licenses/by-nc-nd/4.0/>).

1. Introduction

The risks posed by CO₂, H₂S and other impurities in Natural Gas (NG) are increasingly alarming owing to their negative consequences in humans, equipment and the environment. Natural gas may be classified as sweet or sour. It comprises of methane, ethane, propane, isobutane, n-butane, nitrogen, CO₂, O₂, isopentane, n-pentane, hexane and H₂ [1]. Other gases include helium, hydrogen sulphide and mercaptans which give the gas its characteristic odour. CO₂ and H₂S are the major pollutants in NG. For easy/take transportation, <50 ppm CO₂ is desired [2]. CO₂ and H₂S can be trapped using amine solvents, absorption equipment and membranes [3]. Other contaminants, such as carbonyl sulphide, mercaptans, ethane, pentane etc., are usually removed via distillation and absorption. Gas purification depends on the target-solute solubility, partial vapour pressures of the constituents and the spent heat during solvent recovery [4,5]. Absorption of CO₂ from flue gas using several alcohol-amine solvents has been reported [6].

According to Tang and Zhu [7], the use of amines, carbonates, aqueous ammonia, polymer membranes, ionic liquids and enzymes are recent advances in gas treatment operations. Acid gas removal from contaminated gas depends on the desired application; in internal combustion engines, a CH₄ concentration >90% is friendly [8,9]. High CO₂ in NG reduces engine power [10,11], while >3500 ppm H₂S in gaseous fuels may cause internal erosion of engines [12]. High amount of CO₂ also reduces the burn-rate of natural gas [13]. Transportation of significant amounts of H₂S can cause pipeline corrosion [13], leakages, fire explosions and loss of aquatic and human lives [14] hence, the gas must be treated prior transportation [15]. In selecting a solvent for gas treatment, one must consider its solubility, viscosity, solvent corrosivity, density, thermal stability, % H₂S/CO₂ in feed gas, process economics and solvent recovery [16,17]. According to reports from National Energy Laboratory, the recommended residual sulphur threshold in NG is 0.1 ppm [18]. One popular amine for acid gas absorption is Di-ethanolamine (DEA) with formula HN(CH₂CH₂OH)₂ [19,20]. Natural gas contains significant quantities of H₂S and CO₂ [21] thus, controlling these contaminants is critical in quantifying the risks associated with equipment fouling. Natural gas liquefies at -161 °C and 1 atm which necessitates CO₂ removal [22,23].

Fig. 1 illustrates a traditional gas treatment process (i.e. the Rectisol process) where cold CH₃OH is used to absorb acid gases from

Peer review under responsibility of Egyptian Petroleum Research Institute.

* Corresponding author.

E-mail addresses: adv101000@yahoo.com (S. Eshorame Sanni), oluranti.agboola@covenantuniversity.edu.ng (O. Agboola), omololu.fagbiele@covenantuniversity.edu.ng (O.D. Yusuf), moses.emeterie@covenantuniversity.edu.ng (M.E. Emeterie).