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## Research Article

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# Transient Hydromagnetic Maxwell Fluid Flow over Inclined Stretching Surface with Thermal Radiation, Viscous Dissipation and Ohmic Heating Effects

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**Abstract:** Analysis of an electrically conducting two-dimensional Maxwell fluid flowing through an inclined stretching sheet is considered in this work. Incorporating the viscous dissipation and Ohmic heating effects on the time-dependent optically dense fluid, and using the required similarity transformation variables, the equations governing the flow are deduced and converted into a coupled system of ordinary differential equations. Runge-Kutta fourth order scheme with shooting technique is applied to solve the derived equations. Plots and tables are employed to explain the flow parameters for fluid velocity, temperature, and concentration profiles as well as the skin friction, local Nusselt number, and local Sherwood number. Increase in the angle of inclination parameter, Hartmann number, Prandtl number and Schmidt number reduce the magnitude of the fluid velocity, while radiation parameter, Grashof and Eckert numbers increase it. However, fluid temperature is significantly moderated by Grashof and Prandtl numbers.

**Keywords:** Transient flow, stretching surface, Maxwell fluid, magnetohydrodynamic (MHD), thermal radiation, Runge-Kutta method.

## Introduction

In recent years, the dynamics of non-Newtonian fluids have received considerable attention due to their divergent areas of applications, such as in biological sciences, medical sciences, geophysics, chemical and petroleum industries. The non-linearity ratio between the shear stress and shear rate distinguishes non-Newtonian fluid from Newtonian fluid. In addition, it possesses more complex rheological properties than Newtonian fluid models. Numerous industrially important fluids captured as non-Newtonian are molten plastics, polymers, pulps, mud, pasta, personal care products, ice cream, paints, oils, cheese, asphalt, etc. Due to the complexity of the rheological properties of non-Newtonian fluids, Navier-Stokes' equation has difficulty capturing their mathematical models. Hence, several mathematical models have been developed to account for the divergent features of these fluids. A few of these features include shear thinning, shear thickening, yield stress, stress relaxation etc. The power law model is usually applied to exhibit both the shear thinning and shear thickening effects, the yield stress is addressed by Casson fluid model and the elasticity effect is modeled by grade fluids. Others are micropolar stagnation flows (Odelu and Naresh [1]), Walter's viscoelastic flows (Hussain and Ullah [2]), Jeffrey's viscoelastic boundary layers (Gaffar et al.[3]), Williamson fluids (Megahed.[4]), nanofluid transport from a sphere (Prasad et al. [5]), Eyring-Powell fluid (Gaffar et al. [6]), tangent hyperbolic fluid (Gaffar et al.[7]), and Jeffery nanofluid (Mehmood et al. [8]).

However, these models do not address the effects of stress relaxation, and because a rate-type fluid subclass known as the Maxwell model can predict stress relaxation, it has gained prominence. This model also eradicates the complex impacts of shear-dependent viscosity, making it ideal for concentrating on the effects of a fluid's elasticity on the features of its boundary. Aliakbar et al. [9] investigated the effect of thermal radiation on MHD Maxwell fluid flow over a stretching surface. The effects of thermal radiation and Joule heating on the MHD flow of Maxwell fluid above a stretching sheet were examined by Hayat and Qasim [10]. Heat transfer analysis of time-dependent Maxwell fluid flow over a stretching sheet was studied by Mukhopadhyay [11]. Furthermore, the impact of mass transfer on the Maxwell fluid flow passing through an unsteady stretching sheet was discussed by Mukhopadhyay and Bhattacharyya [12].

Meanwhile, investigations into fluid flow over a stretching surface have experienced a surge in recent decades as a result of its diverse industrial and technological applications, such as metal formation (Altan et al.[13]), polymer extrusion (Fisher [14]) and drawing of plastic films (Tadmor and Klein [15]). Others are metal spinning, glass-fibre production, solidification of liquid crystals, paper production,

petroleum production, exotic lubricants and suspension solutions. Crane [16] initiated the stretching surface flows and obtained the closed form solution of viscous flow over a linearly stretching surface. Crane's work has since been addressed by a number of researchers in a bid to incorporate various aspects of fluid flows and flow configurations. Ishak [17] considered the effect of unsteadiness. Grubka and Bobba [18] studied the impact of variable temperature. Sharidan et al. [19] obtained the similarity solutions for the unsteady boundary layer flow. Chamkha et al. [20] considered porosity, suction/injection and chemical reaction effects, while Eldabe et al. [21] considered three-dimensional flow over a stretching surface. Yusuf et al. [22] investigated Williamson nanofluid over a stretching surface with chemical reaction. Mustafa et al. [23] analysed the unsteady boundary layer flow of a Casson fluid.

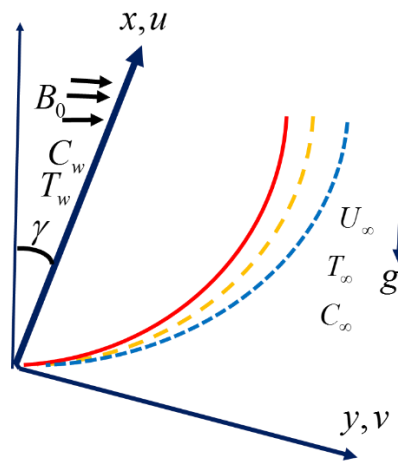
It is worth mentioning that interest in the investigation of thermal radiation effect in a stretching sheet has grown rapidly in the last few decades; due to its relevance in the design of critical equipment such as fins, ceramic and glass manufacturing units, and various propulsion devices for aircraft, missiles, satellites, and space vehicles. In view of the aforementioned applications, Rosseland [24] developed the optically thick approximation for radiation flux. Thereafter, several researchers have since incorporated it into various fluid flows. Hossain and Takhar [25] presented radiation effects on mixed convection flow, and Hossain et al. [26] studied the effect of radiation on free convection from a vertical porous plate. Furthermore, Hossain et al. investigated the effect of radiation on free convection flow. Bataller [27] analysed the radiation effects on the Blasius and Sakiadis flows. Sajid and Hayat [28] investigated the effect of thermal radiation on the boundary layer flow. Gbadeyan and Yusuf [29] examined the effect of nonlinear partial slip and thermal radiation on Oldroyd 8 - constant fluid, and thermal radiation effect on hydromagnetic steady asymmetric flow was considered by Makinde [30].

Despite the numerous benefits of viscous effect in several fields like tribology, instrumentation, food processing, lubrication, polymer manufacturing, etc., it has not been taken into account by several researchers in a variety of hydromagnetic heat and mass transfer flows. However, many fluids' viscosities, vary with temperature. For instance, the viscosity of dry air is  $21.94 \times 10^{-6}$  kg/ms at  $100^{\circ}\text{C}$  and  $26.94 \times 10^{-6}$  kg/ms at  $200^{\circ}\text{C}$ . As a result, it is inappropriate to ignore these vital impact when analyzing fluid flows since doing so could give rise to conclusions that are either under-or over-determined, depending on the situation from using constant viscosity. In view of its significance, Vajravelu and Hadjinicolaou [31] analyzed boundary layer flow over a stretching sheet, taking viscous dissipation into account. Partha et al. [32] examined viscous dissipation effect on the mixed convection flow with heat transfer over an exponentially stretching surface. Sanjayanand and Khan [33] discussed viscous dissipation effect on boundary layer fluid flow over an exponentially stretching surface. Cortell [34] considered the effects of viscous dissipation and thermal radiation on boundary layer flow over a non-linearly stretching sheet. Aziz [35] studied viscous dissipation effect on micropolar fluid over an exponentially stretching sheet. Pavithra and Gireesha [36] presented the effect of viscous dissipation on hydromagnetic fluid flow in a porous medium.

An Ohmic heating (Joule heating) effect is produced when an electrically conducting fluid interacts with an externally applied magnetic field. In other words, it is a process that produces heat when an electric current flows through a conductor. Ohmic heating is used in a variety of industrial and technological processes, which include electric stoves, heaters, incandescent light bulbs, electric fuses, electronic cigarettes, thermistors, food processing, and many others. Devi and Ganga [37] have considered the impacts of viscous and Ohmic heating on hydromagnetic flow problem. Megahed [38] research work considered joule heating and viscous dissipation on magnetohydrodynamic flow past a stretching sheet, and recently, Swain et al. [39] studied viscous dissipation and joule heating effect on hydromagnetic flow past a porous stretching surface. Others are Muhammad et al. [40], Adegbe et al. [41], Osalusi et al. [42], Goud and Nandeppanavar [43], Hasan et al. [44] and Gireesha et al. [45]. The current analysis focuses on the investigation of thermal radiation, viscous dissipation, and Ohmic heating effects on transient hydromagnetic Maxwell fluid over an inclined stretching surface. The findings of this research will be immensely beneficial in the industry for engineers and scientists to boost the efficiency of Maxwell fluid flow during industrial processes.

### **Description of Model**

Consider a two-dimensional incompressible transient hydromagnetic Maxwell fluid over a stretched surface inclined from the vertical with the inclination angle  $\gamma$ , which is coinciding with the plane  $y = 0$ . It is assumed that at  $t < 0$  the flows are steady, however the unsteady heat and mass flows begin at  $t = 0$  with the velocity  $U(x,t) = cx/(1-\alpha t)$ , such that  $c$  and  $\alpha$  are positive constants with dimensions  $(\text{time})^{-1}$ . Note that  $c$  and  $c/(1-\alpha t)$  are the initial stretching and effective stretching rates respectively and are increasing with time. Further assumption is that, a magnetic field with constant strength  $B_0$  is applied in the direction normal to the flow direction, as depicted in Figure 1. The flow is induced by the stretching of the sheet, due to the application of two equal and opposing forces simultaneously along the  $x$ -axis. Keeping the origin constant, the sheet is stretched with a speed that varies linearly with distance from the slit.  $T_w(x,t)$  and  $C_w(x,t)$  are the sheet surface temperature and concentration respectively while the constants free stream temperature and concentration are  $T_\infty$  and  $C_\infty$  respectively, such that  $T_w > T_\infty$  and  $C_w > C_\infty$ . It is assumed that both  $T_w(x,t)$  and  $C_w(x,t)$  vary along the sheet and with time as  $T_w(x,t) = T_\infty + bx(1-\alpha t)^{-2}$ , and  $C_w(x,t) = C_\infty + bx(1-\alpha t)^{-2}$ .



**Fig. 1:** Flow Configuration

Under the aforementioned assumptions, the boundary layer equations of a Maxwell fluid can be stated as (Mukhopadhyay [11]; Mukhopadhyay and Bhattacharyya [12]):

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (1)$$

$$\begin{aligned} \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = & \nu \frac{\partial^2 u}{\partial y^2} - \frac{\sigma B_0^2}{\rho} \left( u + \lambda v \frac{\partial u}{\partial y} \right) \\ & + \lambda \left( u^2 \frac{\partial^2 u}{\partial x^2} + v \frac{\partial^2 u}{\partial y^2} + 2uv \frac{\partial^2 u}{\partial x \partial y} \right) \\ & + g \left[ \beta_r (T - T_\infty) + \beta_c (C - C_\infty) \right] \cos \gamma \end{aligned} \quad (2)$$

$$\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha_c \frac{\partial^2 T}{\partial y^2} + \frac{1}{\rho C_p} \frac{\partial q_r}{\partial y} + \frac{\mu}{\rho C_p} \left( \frac{\partial u}{\partial y} \right)^2 + \frac{\sigma B_0^2 u^2}{\rho C_p} \quad (3)$$

$$\frac{\partial C}{\partial t} + u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = D \frac{\partial^2 C}{\partial y^2} \quad (4)$$

Since the modelled Maxwell fluid is flowing past a stretching surface, the appropriate boundary conditions are:

$$\left. \begin{aligned} u = U_w, v = 0, T = T_w, C = C_w \text{ at } y = 0 \\ u \rightarrow 0, T \rightarrow T_\infty, C \rightarrow C_\infty \text{ at } y \rightarrow \infty \end{aligned} \right\} \quad (5)$$

Note that in the expression above,  $u$  and  $v$  are fluid velocity components along  $x$ -axis and  $y$ -axis respectively.

Introducing the Rosseland approximation for the radiative heat flux which appears in the energy equation as

$$q_r = -\frac{4\sigma^c}{3k^c} \frac{\partial T^4}{\partial y} = -\frac{16\sigma^c T^3}{3k^c} \frac{\partial T}{\partial y}. \quad (6)$$

In Eq. (6),  $T$  is highly non-linear in the energy equation which makes its solution very difficult, hence an assumption of small temperature differences within the flow is taken which helps to linearize the Rosseland formula about the ambient temperature  $T_\infty$ . This means  $T^3$  in Eq. (6) is substituted with  $T_\infty^3$ .

Invoking Eq. (6) in Eq. (3) yields

$$\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha_c \frac{\partial^2 T}{\partial y^2} + \frac{16\sigma^c T_\infty^3}{3\rho C_p k^c} \frac{\partial^2 T}{\partial y^2} + \frac{\mu}{\rho C_p} \left( \frac{\partial u}{\partial y} \right)^2 + \frac{\sigma B_0^2 u^2}{\rho C_p} \quad (7)$$

The following relations are introduced for  $u$ ,  $v$ ,  $\theta$  and  $\phi$ :

$$u = \frac{\partial \psi}{\partial y}, v = -\frac{\partial \psi}{\partial x}, \theta = \frac{T - T_\infty}{T_w - T_\infty}, \phi = \frac{C - C_\infty}{C_w - C_\infty} \quad (8)$$

where  $\psi$  is a stream function. Furthermore, the following similarity transformation variables are introduced

$$\eta = \sqrt{\frac{c}{v(1-\alpha t)}} y, \psi = \sqrt{\frac{vc}{(1-\alpha t)}} x f(\eta), T_w = T_\infty + \frac{cx}{(1-\alpha t)^2} \theta(\eta), C_w = C_\infty + \frac{cx}{(1-\alpha t)^2} \phi(\eta) \quad (9)$$

Employing the relations (9), converts Eqs. (2), (4) and (7) to the following system of coupled ordinary differential equations

$$f''' + ff'' - (f')^2 + A \left( \frac{\eta}{2} f''' + f' \right) - \beta (f^2 f''' - 2ff'f'') - Ha^2 (f' + \beta ff'') - (Gr\theta + Gc\phi) \cos \gamma = 0 \quad (10)$$

$$\frac{1}{Pr} (1 + Nr) \theta'' + f\theta' - f'\theta - A \left( \frac{\eta}{2} \theta' + \theta \right) + Ec(f'')^2 + EcHa^2 (f')^2 = 0 \quad (11)$$

$$\frac{1}{Sc} \phi + f\phi' - f'\phi - A \left( \frac{\eta}{2} \phi' + \phi \right) = 0 \quad (12)$$

Then the boundary conditions in (5) take the form

$$f(0) = 0, f'(0) = 1, \theta(0) = 1, \phi(0) = 0, \quad (13)$$

$$f'(\infty) \rightarrow 1, \theta(\infty) \rightarrow 0, \phi(\infty) \rightarrow 0$$

where

$$A = \frac{\alpha}{c}, \beta = c\lambda_0, \lambda_0 = \frac{\lambda}{1-\alpha t}, Ha = \sqrt{\frac{\sigma B_0^2}{\rho c}},$$

$$Gr = \frac{g\beta_r (T_w - T_\infty)(1-\alpha t)^2}{c^2 x}, Sc = \frac{\nu}{D}, \quad (14)$$

$$Gc = \frac{g\beta_c (C_w - C_\infty)(1-\alpha t)^2}{c^2 x}, Pr = \frac{\nu}{\alpha}, Ec = \frac{c^2 x}{c_p (T_w - T_\infty)(1-\alpha t)^2},$$

$$Nr = \frac{16\sigma^c T_\infty^3}{3k^c k}, Re_x = \frac{U_w x}{\nu}$$

Next are expressions for the skin friction coefficient, heat and mass transfer fluxes at the wall in dimensionless form, these are expressed as:

$$C_f \text{Re}_x^{\frac{1}{2}} = f''(0); \text{Re}_x^{-\frac{1}{2}} Nu_x = -(1 + Nr)\theta'(0); \text{Re}_x^{-\frac{1}{2}} Sh_x = -\phi'(0) \quad (15)$$

### Method of Solution Via Runge-Kutta/Shooting Technique

To apply the Runge-Kutta/Shooting technique, the model Eqs. (10) - (12) together with the boundary conditions (13) are converted to a set of first order initial value problems. Let,

$$y_1 = f, y_2 = f', y_3 = f'', y_4 = \theta, y_5 = \theta', y_6 = \phi, y_7 = \phi' \quad (16)$$

Then in view of Eq. (16), Eqs. (10)-(13) assume the form:

$$\left. \begin{aligned} y_1' &= y_2, y_1(0) = 0 \\ y_2' &= y_3, y_2(0) = 1 \\ y_3' &= \frac{1}{(1 - \beta y_1^2)} \left[ y_1 y_3 - y_2^2 + A \left( \frac{\eta}{2} y_3 + y_2 \right) + 2\beta y_1 y_2 y_3 \right. \\ &\quad \left. - Ha^2 (y_2 + \beta y_1 y_3) + (Gr y_4 + Gc y_6) \cos \gamma \right], y_3(0) = L_1 \\ y_4' &= y_5, y_4(0) = 1 \\ y_5' &= - \left( \frac{Pr}{1 + Nr} \right) \left[ y_1 y_4 - y_2 y_4 - A \left( \frac{\eta}{2} y_5 + y_4 \right) \right. \\ &\quad \left. + Ec (y_3^2 + Ha^2 y_2^2) \right], y_5(0) = L_2, \\ y_6' &= y_7, y_6(0) = 1, \\ y_7' &= -Sc \left[ y_1 y_6 - y_2 y_6 - A \left( \frac{\eta}{2} y_7 + y_6 \right) \right], y_7(0) = L_3 \end{aligned} \right\} \quad (17)$$

The fourth-order Runge-Kutta method is employed on Maple 18 see Rana and Shukla [46] and El-Aziz and Nabil [47] for more on MAPLE software) to obtain the solutions to Eqs (17). A step size of 0.001 is used to calculate the equations' solutions. At a distance where the influence of boundary layers is less substantial, the results are truncated. To verify the validity of the current numerical method, the results have been compared to previously published works in the literature. Thus, in Tables 1, 2 and 3 the results are compared with Grubka and Bobba [18], Ishak [17], Sharidan et al. [19] and Chamkha et al. [20] respectively. In all these, the results demonstrate excellent agreement.

### Results and Discussion

Transient MHD Maxwell fluid flow over a stretching surface with thermal radiation, viscous dissipation and Ohmic heating effects has been investigated. For some dimensionless physical values, computed results are presented in Tables 1-3 and Figs. 2-10. The values of the pertinent flow parameters are fixed throughout the analysis except otherwise stated in the figures and tables. These are  $A=1$ ,  $\beta=0.1$ ,  $Nr=0.1$ ,  $Gr=1$ ,  $Gc=1$ ,  $\gamma=\pi/6$ ,  $Sc=0.62$ ,  $Pr=1$ ,  $Ha=0.5$ ,  $Ec=0.1$ ,  $f_w=0$ .

**Table 1:** Comparison of  $-\theta'(0)$  for various values of  $A, H, Pr$  for  $\beta=0, \gamma=90^\circ$

$A$	$H$	$Pr$	Grubka and Bobba [18]	Ishak [17]	Present
0	0	0.01	0.0197	0.0197	0.1122
		0.72	0.8086	0.8086	0.8088364017
		1	1.0000	1.0000	1.0000083024
		3	1.9237	1.9237	1.9236723873
		6.7		3.0003	3.0002573873
		10	3.7207	3.7207	3.7206520234
		100	12.2940	12.2940	12.294080769

	1	0.01	0.0140	0.1092151587
		0.7	0.68967	0.6915395368
		1	0.8921	0.8924194639
		10	3.6170	3.6169754359
		100	12.194	12.194108365
1	0	0.7	1.0834	1.0833883410
		7	3.7682	3.7682403394
	1	0.7	1.0500	1.0499871879
		7	3.7164	3.7164750608

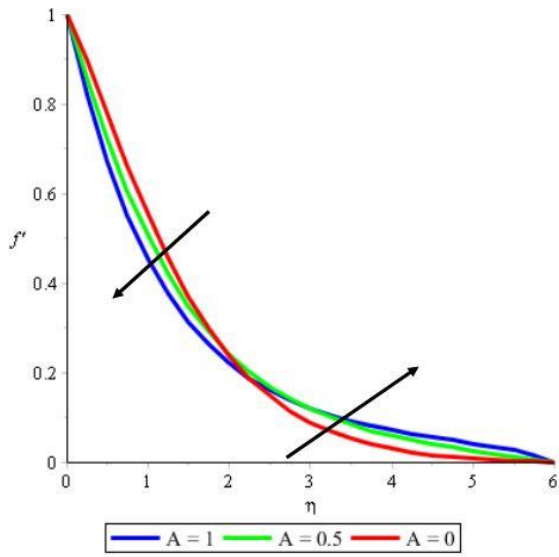
**Table 2:** Comparison of  $-f''(0)$  with Sharidan et al. and Chamkha et al. [20]  $\beta = 0, H = 0, \gamma = 90^\circ, Pr = 1$

A	Sharidan et al. [19]	Chamkha et al.[20]	Present
0.8	1.261042	1.261512	1.2610468
1.2	1.377722	1.378052	1.3777344

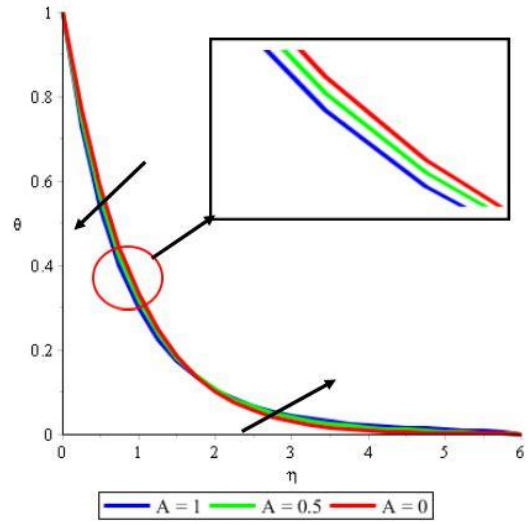
**Table 3:** Comparison of  $-f''(0)$ ,  $-\theta'(0)$  and  $-\phi'(0)$  for various values of A, Pr and Sc at  $\gamma = 1, K/H = 1$ ,  $Gr = 1, Gc = 2, f_w = 0.5$

A	Pr	Sc	Chamkha et al. [20]			Present		
			$-f''(0)$	$-\theta'(0)$	$-\phi'(0)$	$-f''(0)$	$-\theta'(0)$	$-\phi'(0)$
0	0.71	0.22	0.27377	1.158393	0.74014	0.273514	1.157477	0.739461
		0.60	0.49677	1.101087	1.312248	0.496533	1.100159	1.311761
		0.94	0.59941	1.076931	1.713443	0.599134	1.076292	1.713094
	0.3	0.62	0.38639	0.62198	1.355045	0.386548	0.621810	1.354616
		0.71	0.50438	1.099032	1.337571	0.505057	1.098321	1.337270
		1	0.55244	1.384875	1.331027	0.552362	1.394657	1.330859
0	0.71	3	0.69042	2.966999	1.316710	0.690086	2.965405	1.316382
		0.62	0.50438	1.099032	1.337571	0.504057	1.098321	1.337270
		1	0.88473	1.324178	1.496687	0.884328	1.323532	1.496483
	2	1.215097	1.526933	1.648849	1.214068	1.526815	1.648229	
		10	2.830195	2.656791	2.599922	2.829416	2.656700	2.599545

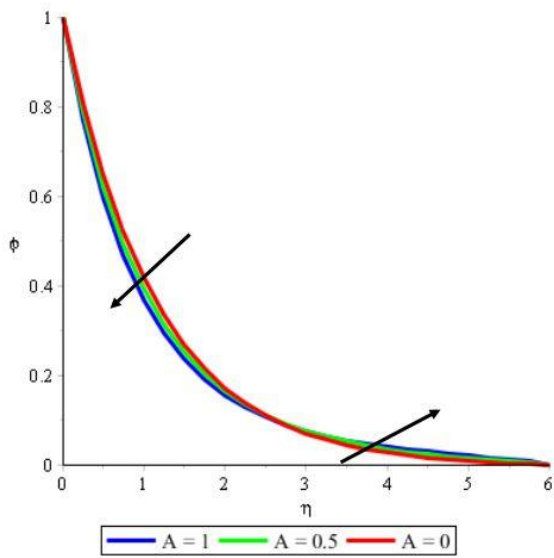
Figures 2a, 2b and 2c indicate a reduction in fluid velocity near the wall while a rise is registered away from the wall. The momentum and thermal boundary layer thicknesses as well as mass transfer rate decrease as depicted by the plots, which causes the reduction in fluid velocity, temperature, and concentration. In addition, the unsteadiness parameter is a function of fluid thermal diffusivity, that is,  $A = \alpha/c$ . Increasing the unsteadiness parameter, the fluid thermal diffusivity increases, hence the velocity, temperature and concentration profiles decrease. It is further observed that an opposing trend is displayed in the figures for the free stream region. Next is the influence of inclination parameter ( $\gamma$ ), fluid motion is lessened while the temperature and concentration profiles receive a boost as displayed in Fig. 3. Varying the inclination angle as  $10^\circ, 45^\circ, 75^\circ$  reduces the impact of gravitational force on the flow, resulting in a drastic reduction in buoyancy force effect, hence the reduction in the fluid motion. This can be compared to when the stretching sheet is vertically downward at  $\gamma = 0^\circ$ , which allows the maximum impact of gravitational force and fluid maximum flow motion. However, fluid temperature and concentration profiles increase due to thermal and concentration boundary layer thicknesses.



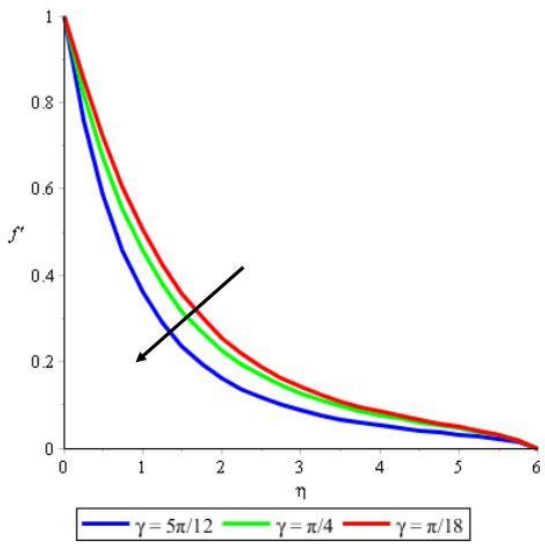
**Fig. 2a** Velocity, for various values of  $A$



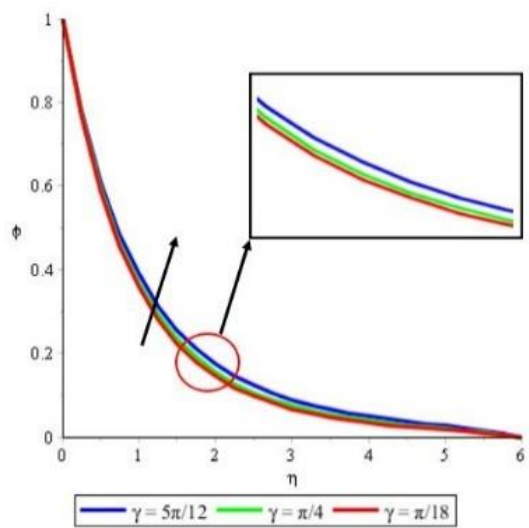
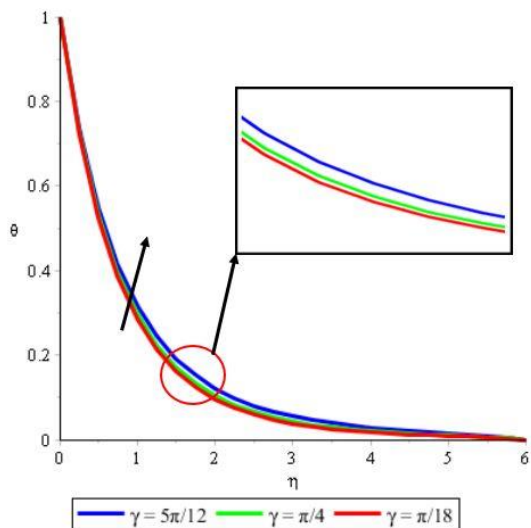
**Fig. 2b** Temperature for various values of  $A$



**Fig. 2c** Concentration for various values of  $A$ .



**Fig. 3a** Velocity for various values of



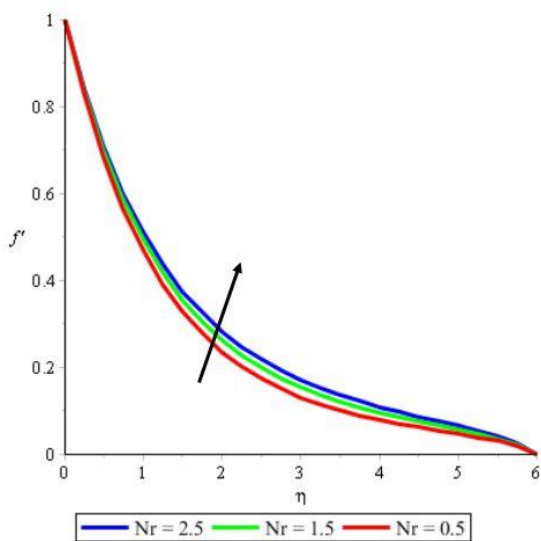


**Fig. 3b** Temperature for various values of  $\gamma$

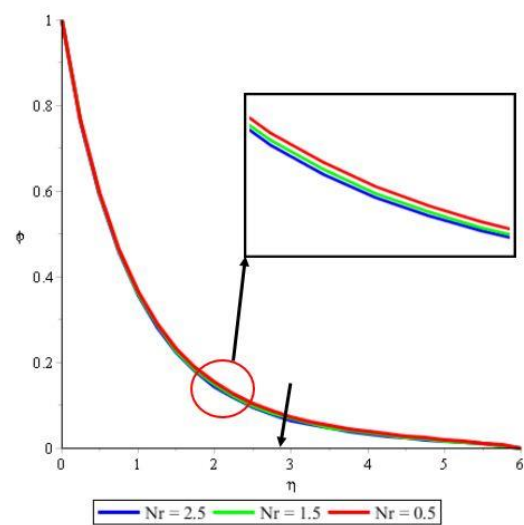
**Fig. 3c** Concentration for various values of  $\gamma$

Response of velocity, temperature and concentration profiles to variation in radiation parameter is presented in Figs. 4a, b and c. An increment in fluid velocity and temperature is noticed while fluid concentration is lowered. This happens as a consequence of a decrease in the mean absorption coefficient,  $k^c$  as the radiation parameter  $Nr (= 16\sigma^c T_\infty^3 / 3k^c k)$  receives a boost. Consequently, the fluid's rate of radiative heat transfer is rising, leading to a decline in fluid velocity and temperature. However mass concentration is lowered due to a reduction in concentration boundary layer thickness.

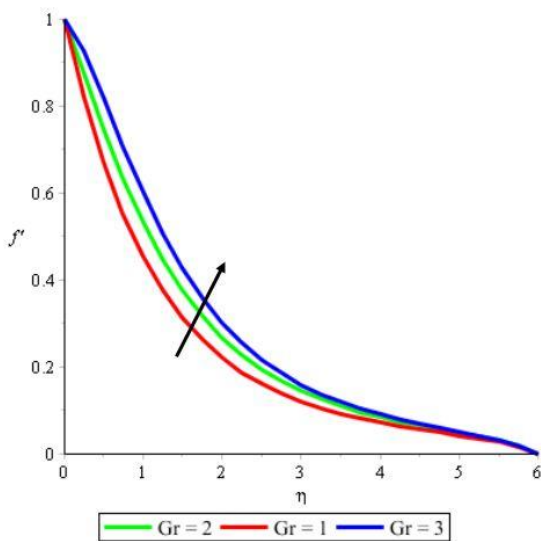
Figures 5 and 6 depict the effects of Grashof numbers ( $Gr$ ,  $G_c$  -thermal and concentration buoyancy forces, respectively) on fluid velocity, temperature and concentration profiles. Since Grashof number expresses the buoyant-to-viscous force ratio, physically speaking,  $Gr > 0$  denotes heating of the fluid or cooling of the wall, whereas  $Gr < 0$  implies cooling of the fluid or heating of the sheet surface. Therefore, increasing the values of Grashof numbers reduces fluid viscosity. This in effect raises fluid motion but cools the fluid temperature and concentration profiles.



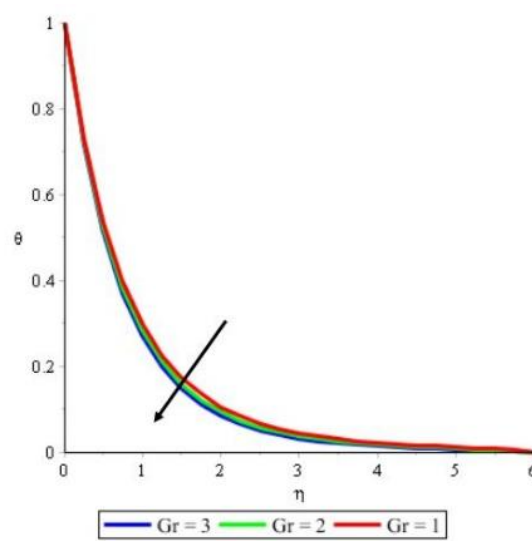
**Fig. 4** Velocity for various values of  $Nr$



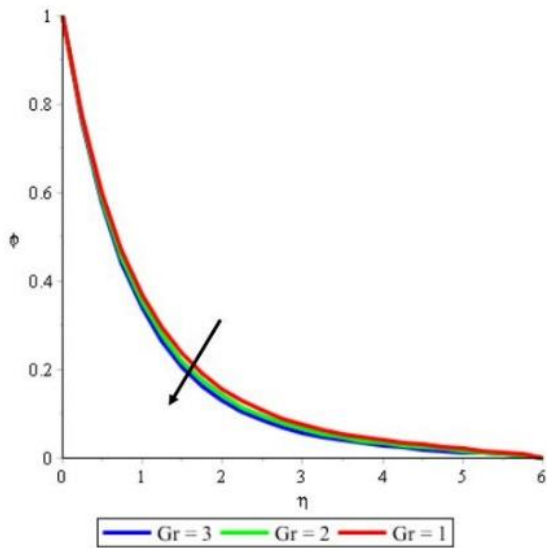
**Fig. 4c** Concentration (c) for various values of  $Nr$



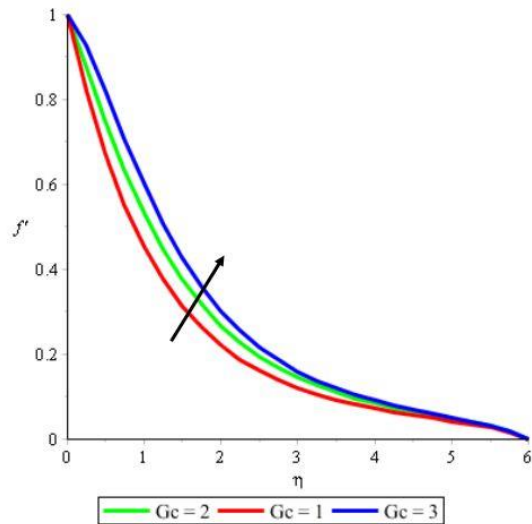
**Fig. 5a** Velocity for various values of  $Gr$



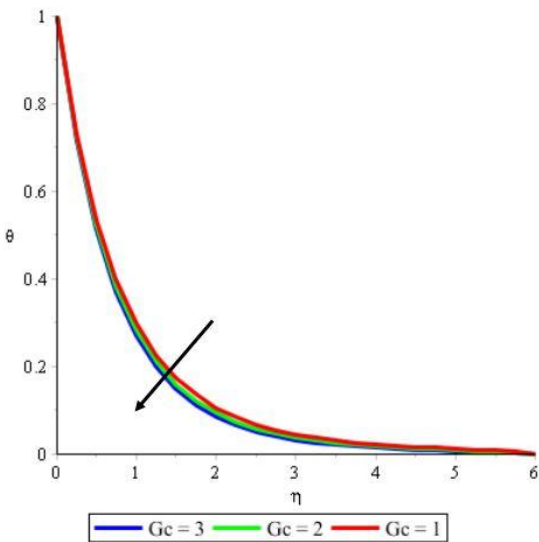
**Fig. 5b** Temperature for various values of  $Gr$



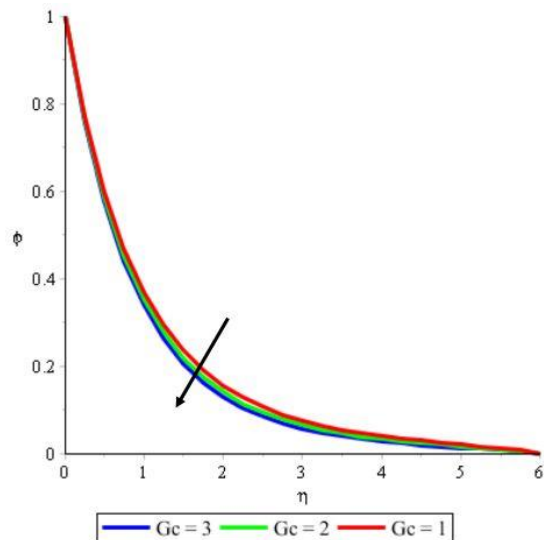
**Fig. 5c** Concentration for various values of  $Gr$  .



**Fig. 6a** Velocity for various values of  $Gc$  .



**Fig. 6b** Temperature for various values of  $Gc$  .

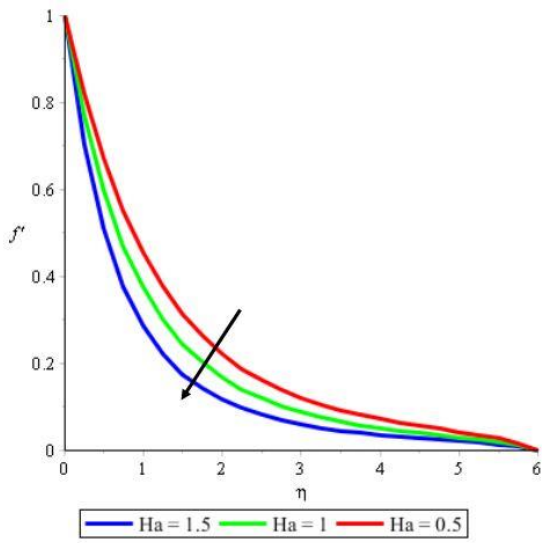


**Fig. 6c** Concentration for various values of  $Gc$  .

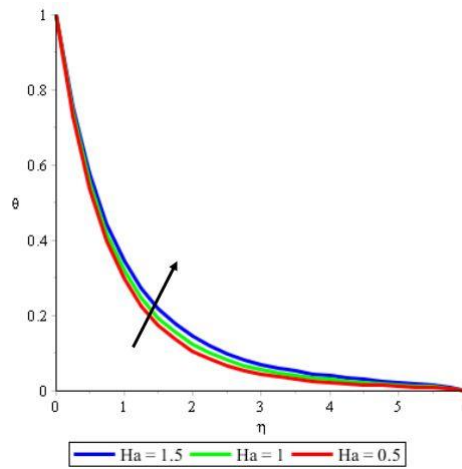
In Fig. 7, magnetic field parameter effects on fluid velocity, temperature and concentration are respectively displayed. Fluid velocity drops as the magnetic field parameter value is enhanced. An opposing Lorentz force is generated in an electrically conducting fluid when a magnetic field in a transverse direction to the flow is introduced. As the magnetic field value increases, the fluid velocity decreases as a result of this resistive force's tendency to slow the flow, as displayed in Fig. 7a. However, in Figs. 7b and 7c, an increase is observed in fluid temperature and concentration. This is because Ohmic heating (or Lorentz heating resulting from a magnetic field), which is present in the energy equation, acts as an additional heat source for the flow system, raising the fluid's temperature.

As depicted in Fig. 8, Prandtl number variation has a significant impact on fluid velocity, temperature and concentration profiles. It is observed that a reduction in fluid velocity and temperature is registered while species concentration is enhanced. Physically speaking, this is correct since Prandtl number relates fluid momentum diffusivity to thermal diffusivity. Increasing the value of the Prandtl number from 0.71 to 2 leads to a drop in fluid motion. This is due to a reduction in momentum boundary layer thickness, hence the momentum diffusivity, leading to a reduction in fluid velocity as depicted in Fig. 8a. Furthermore, in Fig. 8b fluid temperature is observed to have significantly reduced. There is a massive increase in fluid thermal conductivity for smaller values of Prandtl number. Therefore, more

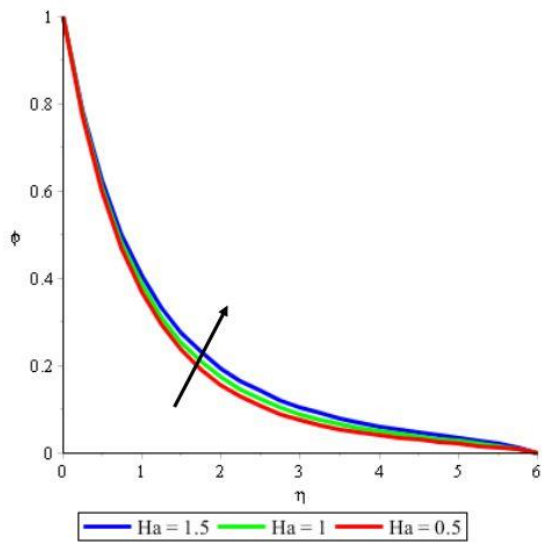
heat diffuses away from the sheet for reducing values of Prandtl than for its increment. However, species concentration is observed to have improved, as displayed in Figure 8c.



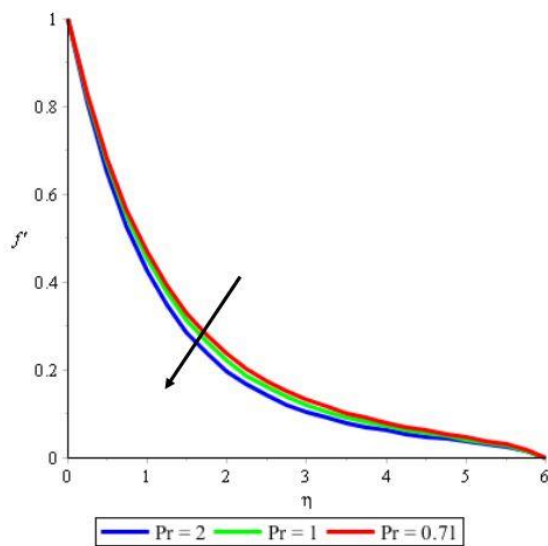
**Fig. 7a** Velocity for various values of  $Ha$  .



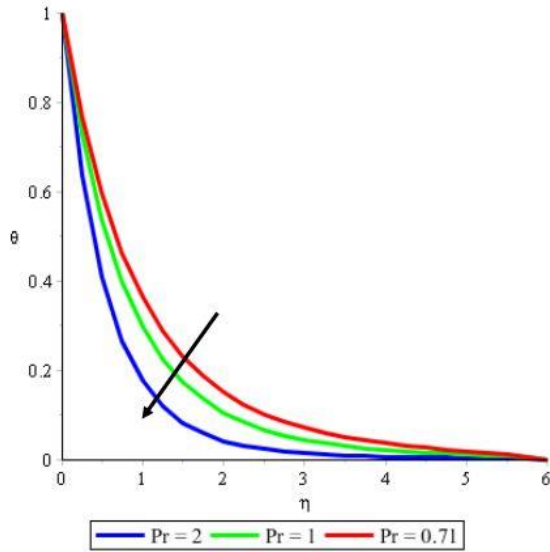
**Fig. 7b** Temperature for various values of  $Ha$  .



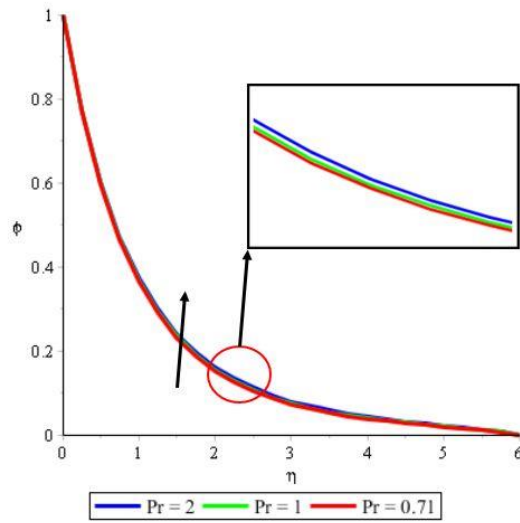
**Fig. 7c** Concentration for various values of  $Ha$  .



**Fig. 8a** Velocity for various values of  $Pr$  .

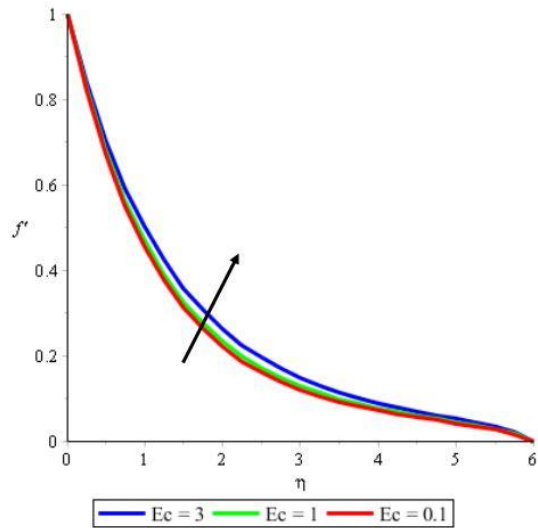


**Fig. 8b** Temperature for various values of  $Pr$  .

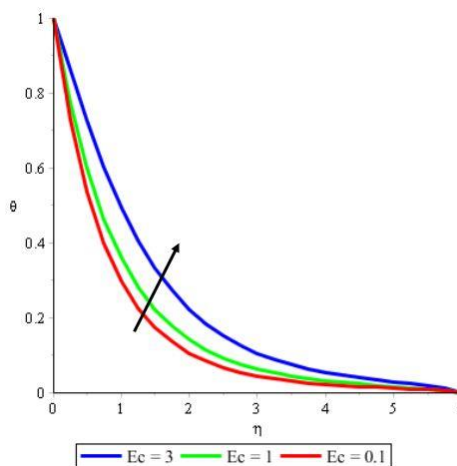


**Fig. 8c** Concentration for various values of  $Pr$  .

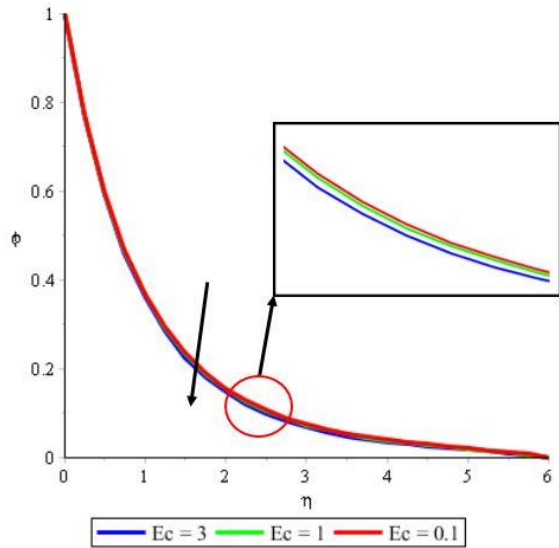
The Eckert number improves fluid velocity and temperature while the concentration profile is reduced, as displayed in Fig. 9. Eckert number describes the interaction between the fluid's enthalpy and kinetic energy in the flow. It depicts the process by which kinetic energy is transformed into internal energy as a result of work done against viscous fluid stresses. Therefore, fluid velocity and temperature increase while concentration boundary layer thickness decreases as viscous dissipative heat increases. In Fig. 10, fluid motion and species concentration are observed to have reduced while the temperature increases as Schmidt number is enhanced. The relationship between fluid kinematic viscosity and mass diffusivity is the quantity that is designated as Schmidt number ( $Sc$ ) in the concentration equation. It explains the association between the relative thickness of the mass-transfer boundary layer and the hydrodynamic boundary layer. Consequently, a rise in the Schmidt number renders the fluid more viscous, resulting in a reduction in fluid motion and concentration while the temperature is raised.



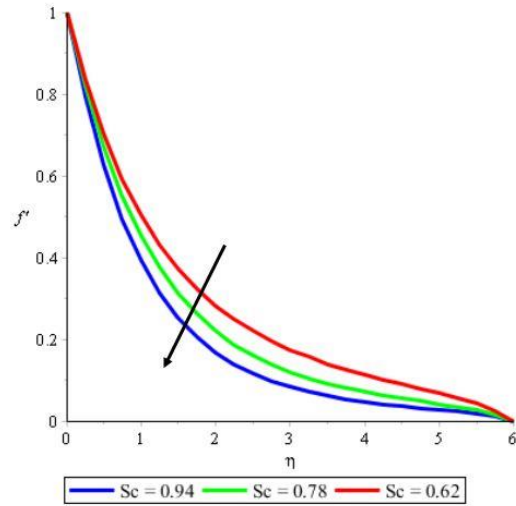
**Fig. 9a** Velocity for various values of  $Ec$  .



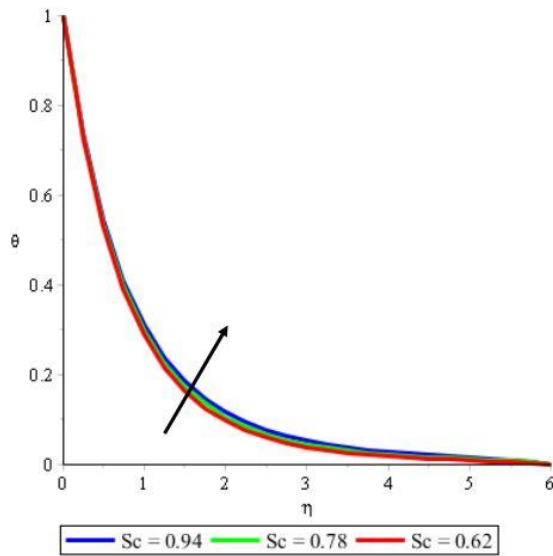
**Fig. 9b** Temperature for various values of  $Ec$  .



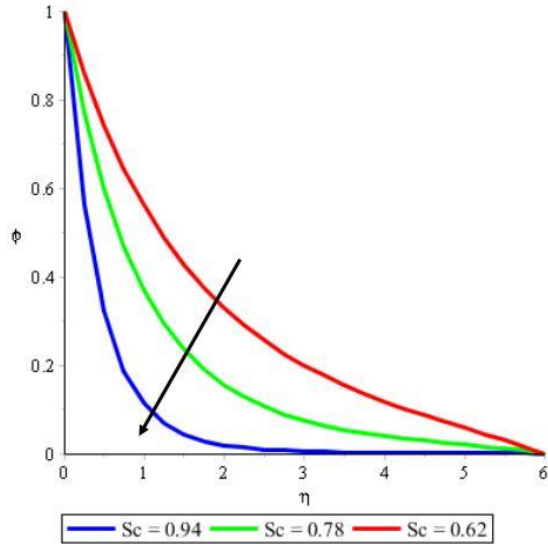
**Fig. 9c** Concentration for various values of  $Ec$  .



**Fig. 10a** Velocity for various values of  $Sc$



**Fig. 10b** Temperature for various values of  $Sc$



**Fig. 10c** Concentration for various values of  $Sc$

## CONCLUSIONS

The current study presents the electrically conducting two-dimensional Maxwell fluid flow through a stretching sheet. Viscous dissipation, inclination angle, Ohmic heating and unsteadiness parameter are incorporated in the optically dense fluid. By applying Runge-Kutta/Shooting technique, numerical solutions are obtained for the ordinary differential equations. Comparing the current findings with the literature that is already available, it is demonstrated that there is good agreement. The following are the key findings:

- Flow motion is decelerated by inclination angle, magnetic field parameters and Prandtl number. However, radiation parameter, Grashof and Eckert numbers accelerated it,
- Fluid temperature is heightened by inclination, radiation and magnetic field parameters. However, Grashof and Prandtl numbers cool the system,
- Concentration of species is enhanced by inclination angle parameter, magnetic field parameter and Prandtl number,
- Heat transfer rate is enhanced by Prandtl number and unsteadiness parameter.

## ACKNOWLEDGEMENTS

## NOMENCLATURE

$a, b, c$	constants
$A$	unsteadiness parameters
$B_0^2$	uniform transverse magnetic field
$C_p$	specific heat of the fluid at constant temperature (J/kg·K)
$C_w$	concentration of sheet surface
$C_\infty$	free-stream concentration
$D$	coefficient of mass diffusivity
$Ec$	Eckert number
$f$	dimensionless stream function
$g$	<i>acceleration due to gravity</i>
$Gr$	local Grashof number due to temperature differences
$Gc$	local Grashof number due to concentration differences
$Ha^2$	Hartman number
$k$	thermal conductivity (W/m·K)
$k^c$	absorption coefficient
$Nr$	radiation parameter
$Pr$	Prandtl number
$q_r$	Relative heat flux
$Re$	Local Reynolds number
$T$	temperature of the fluid (K)
$T_w$	temperature of the sheet surface
$T_\infty$	free-stream temperature
$Sc$	Schmidt number
$u$	velocity component along $x$ direction
$v$	velocity component along $y$ direction
<i>Greek Symbols</i>	
$\alpha^c$	thermal diffusivity
$\beta$	Maxwell parameter
$\beta_c$	solubility expansion coefficient
$\beta_T$	thermal expansion coefficient
$\gamma$	inclination angle
$\eta$	similarity variable
$\theta$	dimensionless temperature
$\lambda$	relaxation time parameter of the fluid
$\lambda_0$	constant
$\mu$	dynamic viscosity
$\nu$	kinematic viscosity
$\rho$	fluid density (kg/m <sup>3</sup> )
$\sigma$	electrical conductivity
$\sigma^c$	Stefan Boltzmann constant
$\psi$	stream function

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